

# Lecture # 11: Particle image velocimetry

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***Dr. Hui Hu***

***Martin C. Jischke Professor in Aerospace Engineering***

***Department of Aerospace Engineering, Iowa State University***

***Howe Hall - Room 2251, 537 Bissell Road, Ames, Iowa 50011-1096***

***Tel: 515-294-0094 (O) / Email: [huhui@iastate.edu](mailto:huhui@iastate.edu)***

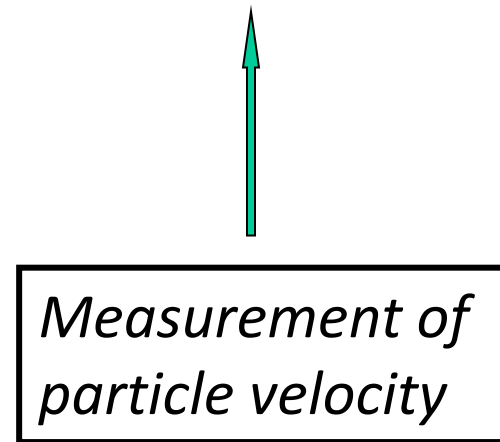
**Sources/ Further reading:**

Raffel, Willert, Wereley, Kompenhans, "Particle image velocimetry: A practical guide" 2<sup>nd</sup> ed.

# Particle-based Flow Diagnostic Techniques

- Seeded the flow with small particles ( $\sim \mu\text{m}$  in size)
- **Assumption:** the particle tracers move with the same velocity as local flow velocity!

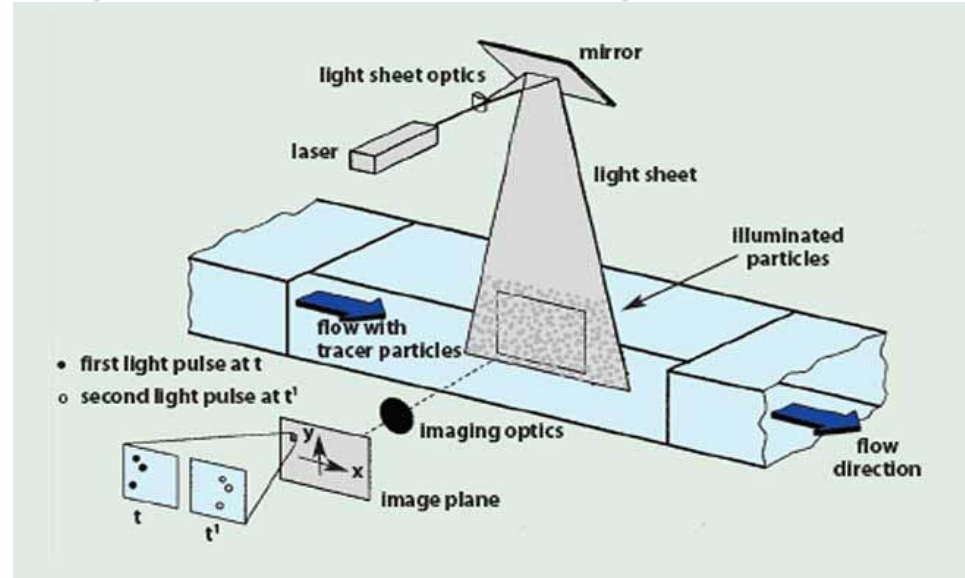
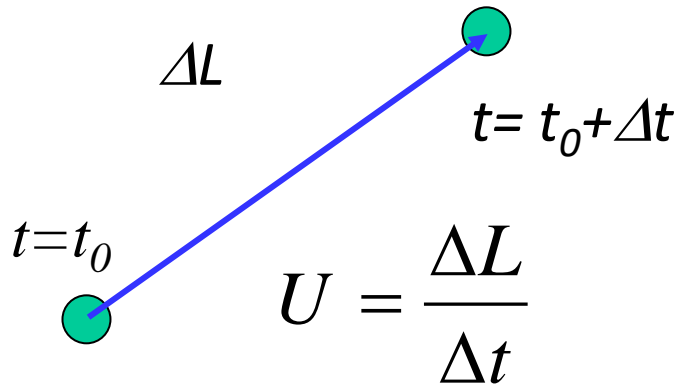
$$\boxed{\begin{array}{c} \text{Flow velocity} \\ V_f \end{array}} = \boxed{\begin{array}{c} \text{Particle velocity} \\ V_p \end{array}}$$



- **Smoke visualization**

# Particle Image Velocimetry (PIV) technique

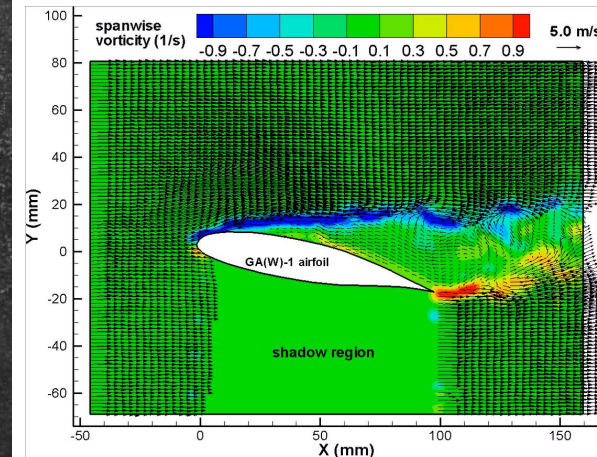
- Time-of-flight method:** to measure the displacements of the tracer particles seeded in the flow in a fixed time interval.



a.  $T = t_0$



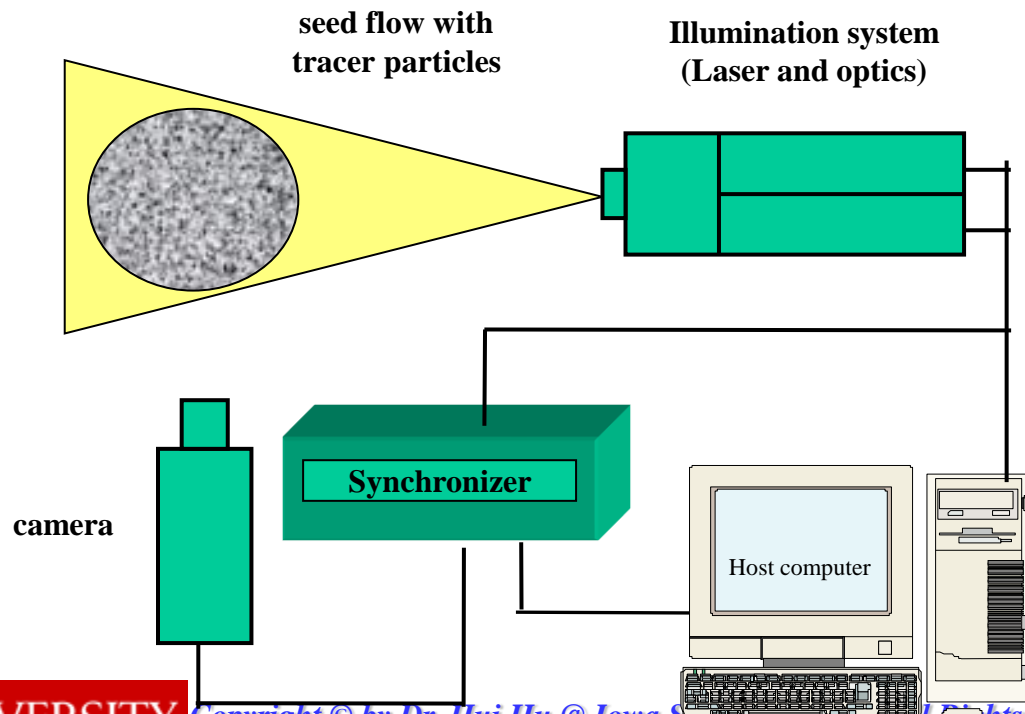
b.  $T = t_0 + 10 \mu s$



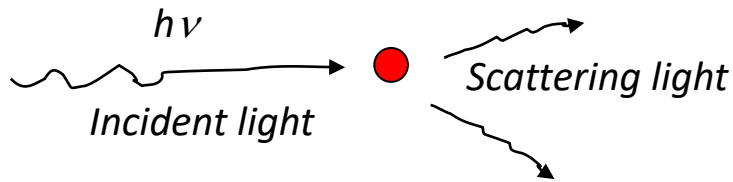
Corresponding Velocity field

# PIV System Setup

- Particle tracers: track the fluid movement.
- Illumination system: illuminate the flow field in the interest region.
- Camera: capture the images of the particle tracers.
- Synchronizer: control the timing of the laser illumination and camera acquisition.
- Host computer: to store the particle images and conduct image processing.



# Tracer Particles for PIV



Particle  $< \frac{1}{10}\lambda$   
( $< 50\text{nm}$ )  
Rayleigh's  
Scattering



$$Q \propto \frac{r}{\lambda}$$

$\frac{1}{10}\lambda < \text{Particle} < \lambda$   
( $50\text{-}500\text{nm}$ )  
Mie Scattering



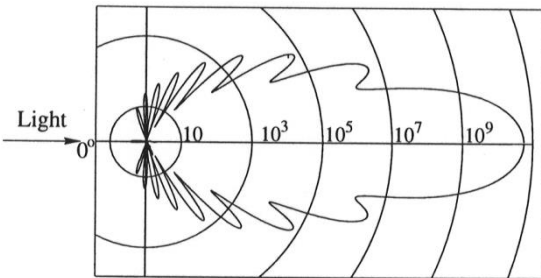
$$Q \propto C + \cos\left(\frac{r}{f}\right) e^{-k\left(\frac{r}{f}\right)}$$

Particle  $> \lambda$   
( $> 1\mu\text{m}$ )  
Optical  
Scattering

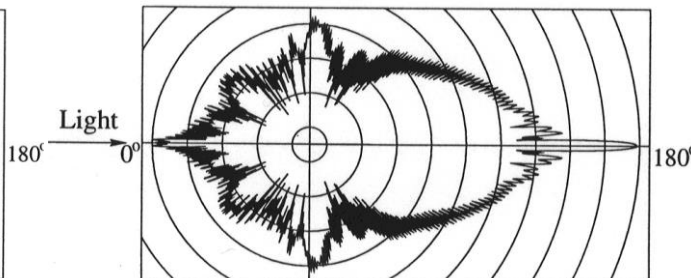


$$Q \propto C$$

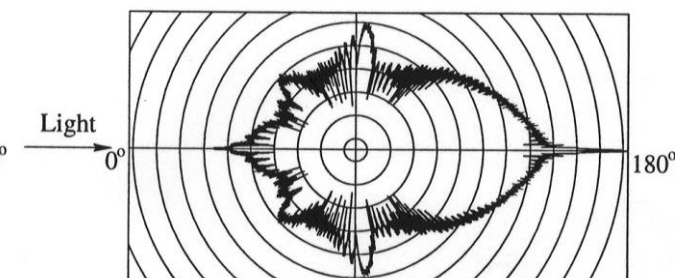
- Tracer particles should be **neutrally buoyant** and **small enough** to follow the flow **perfectly**.
  - Tracer particles should be **big enough** to **scatter** the illumination lights **efficiently**.
  - The scattering efficiency of trace particles also strongly depends on the ratio of the **refractive index** of the particles to that of the fluid.
- For example: the refractive index of **water** is considerably larger than that of **air**. The scattering of particles in air is at least one order of magnitude more efficient than the same particles size in water.



a).  $d=1\mu\text{m}$



b).  $d=10\mu\text{m}$



c).  $d=30\mu\text{m}$

# Tracer Particles for PIV

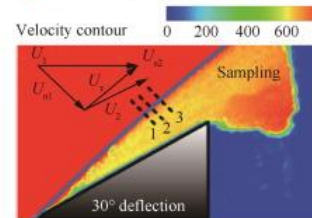
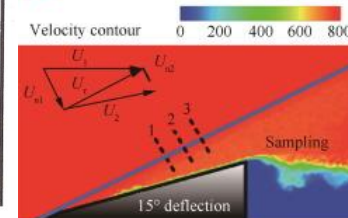
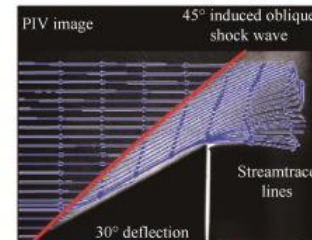
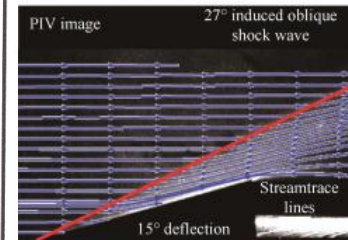
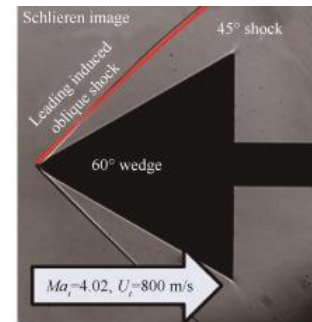
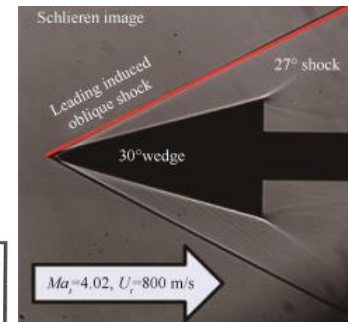
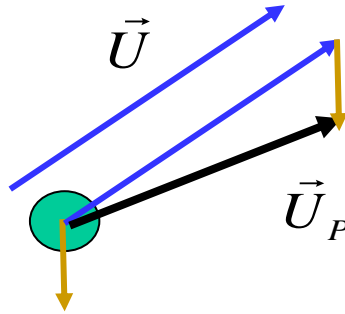
- A primary source of measurement error is the influence of gravitational forces when the density of the tracer particles is different to the density of work fluid.
- The velocity lag of a particle in a continuously acceleration fluid will be:

$$U_g = d_p^2 \frac{(\rho_p - \rho)}{18\mu} g$$

$$\vec{U}_s = \vec{U}_p - \vec{U} = d_p^2 \frac{(\rho_p - \rho)}{18\mu} g$$

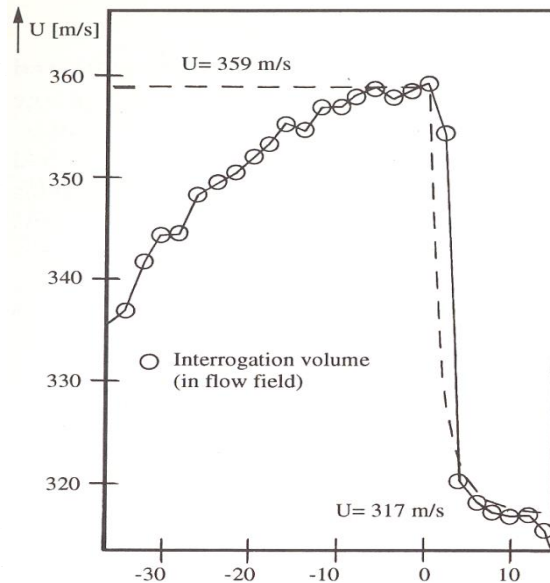
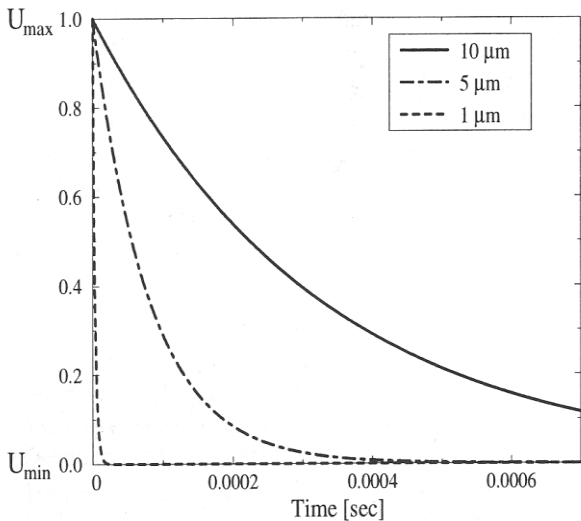
$$\vec{U}_p(t) = \vec{U}(1 - \exp(-\frac{t}{\tau_s}));$$

$$\tau_s = d_p^2 \frac{\rho_p}{18\mu}$$



(a) A wedge with deflection angle 15°

(b) A wedge with deflection angle 30°



# Tracer Particles for PIV

- *Tracers for PIV measurements in liquids (water):*

- *Polymer particles ( $d=10\sim 100\ \mu\text{m}$ , density =  $1.03 \sim 1.05\ \text{kg}/\text{cm}^3$ )*
- *Silver-covered hollow glass beads ( $d = 1 \sim 10\ \mu\text{m}$ , density =  $1.03 \sim 1.05\ \text{kg}/\text{cm}^3$ )*
- *Fluorescent particle for micro flow ( $d=200\sim 1000\ \text{nm}$ , density =  $1.03 \sim 1.05\ \text{kg}/\text{cm}^3$ ).*
- *Quantum dots ( $d= 2 \sim 10\ \text{nm}$ )*

- *Tracers for PIV measurements in gaseous flows:*

- *Smoke ...*
- *Droplets, mist, vapor...*
- *Condensations ....*
- *Hollow silica particles ( $0.5 \sim 2\ \mu\text{m}$  in diameter and  $0.2\ \text{g}/\text{cm}^3$  in density for PIV measurements in combustion applications.*
- *Nanoparticles of combustion products*

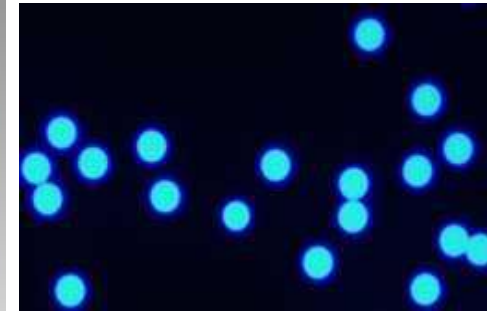
## Product

Polyamide particles,  $55\ \mu\text{m}$ ,  $1.2\ \text{g}/\text{cm}^3$

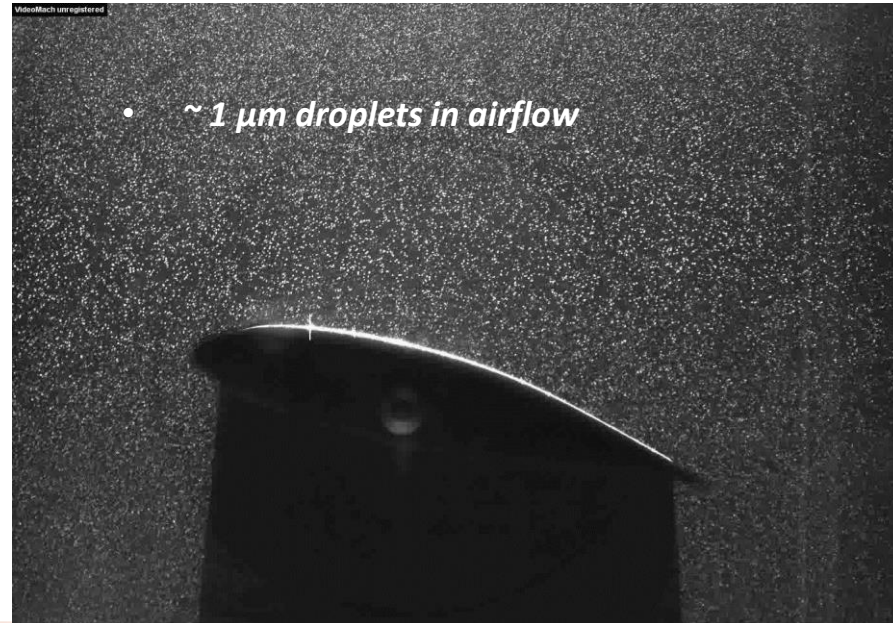
Polyamide particles,  $100\ \mu\text{m}$ ,  $1.1\ \text{g}/\text{cm}^3$

Polyamide particles HQ,  $20\ \mu\text{m}$ ,  $1.03\ \text{g}/\text{cm}^3$

Polyamide particles HQ,  $60\ \mu\text{m}$ ,  $1.03\ \text{g}/\text{cm}^3$

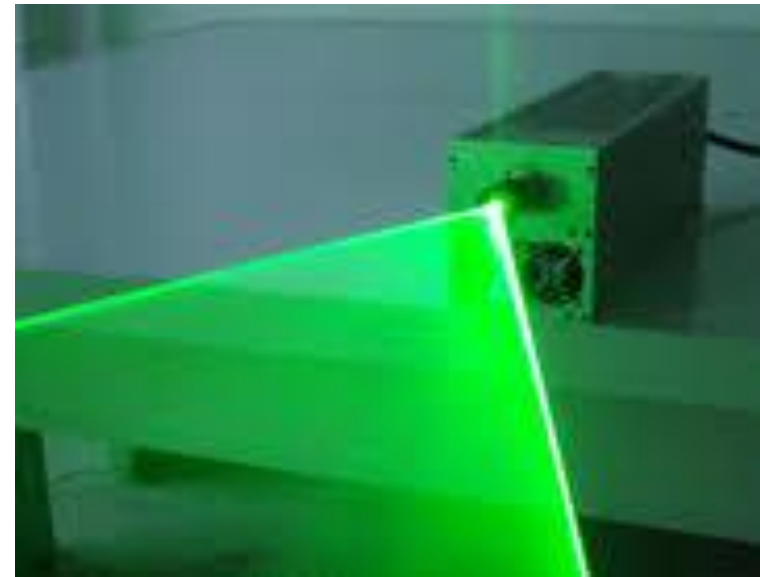
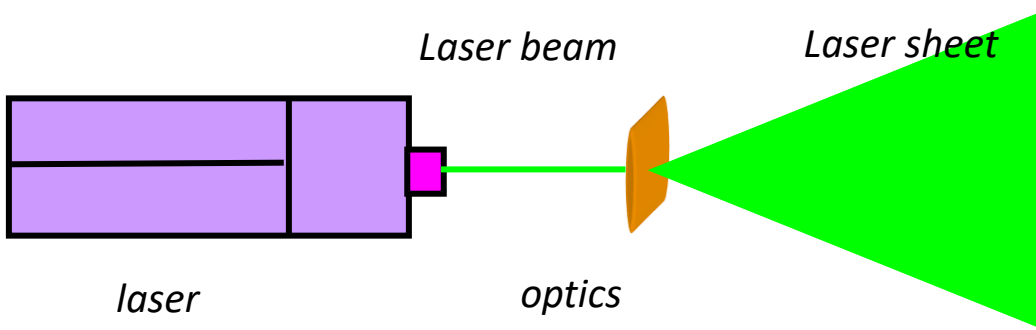


- *Fluorescent particle*



# illumination system

- *The illumination system of PIV is always composed of light source and optics.*
- **Lasers:** such as Argon-ion laser and Nd:YAG Laser, are widely used as light source in PIV systems due to their ability to **emit monochromatic light** with **high energy density** which can easily be bundled into thin light sheet for illuminating and recording the tracer particles without chromatic aberrations.
- **Optics:** always consisted by a set of cylindrical lenses and mirrors to shape the light source beam into a planar sheet to illuminate the flow field.





# Double-pulsed Nd:Yag Laser for PIV

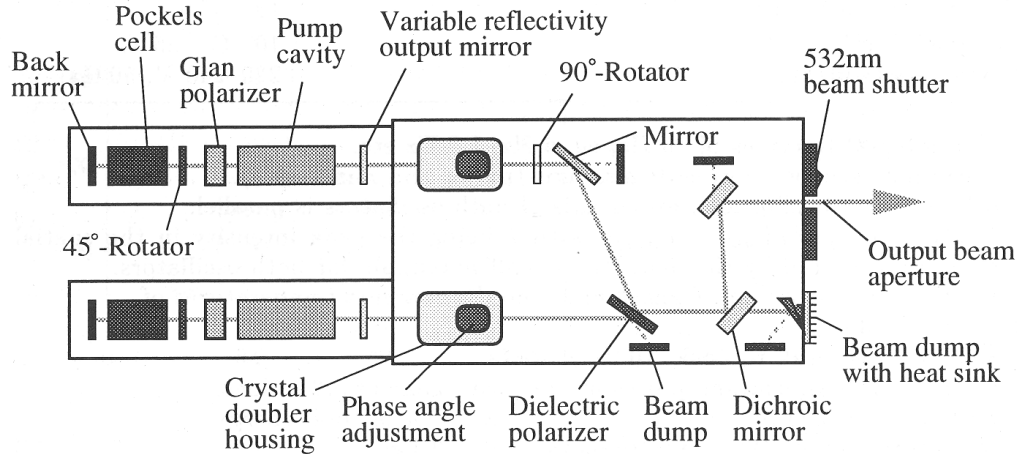


Fig. 2.17. Double oscillator laser system with critical resonators

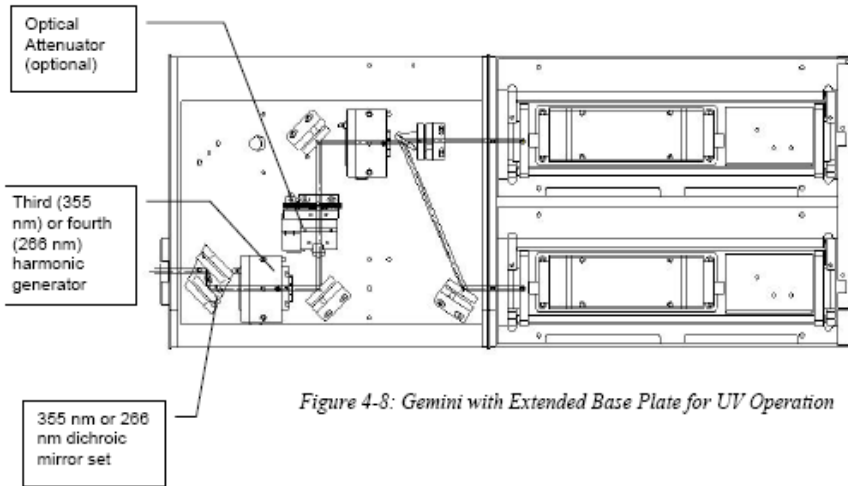
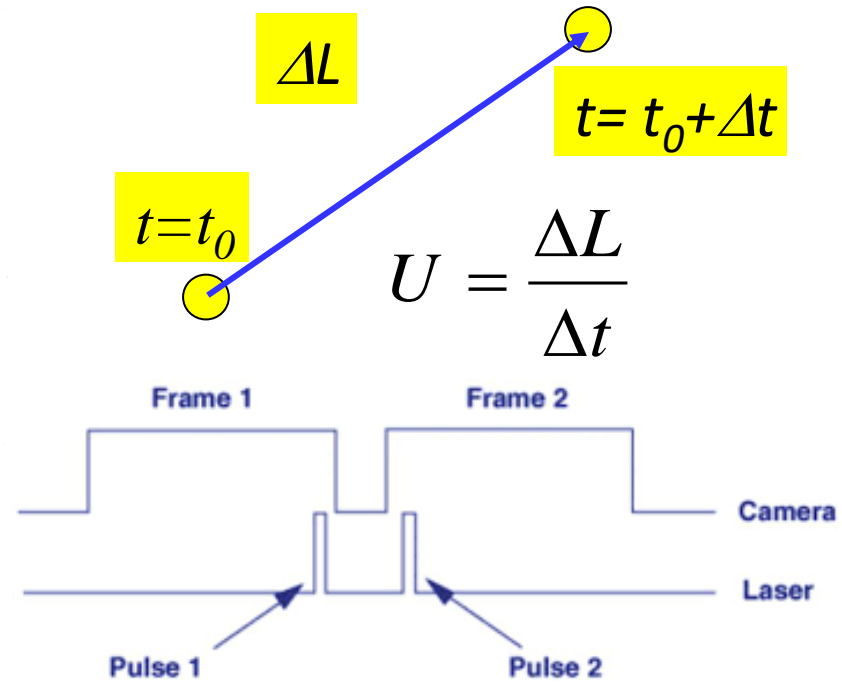
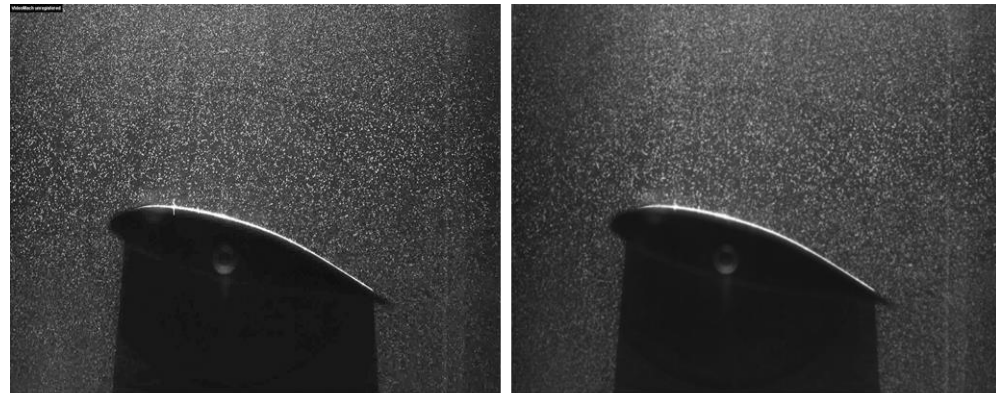


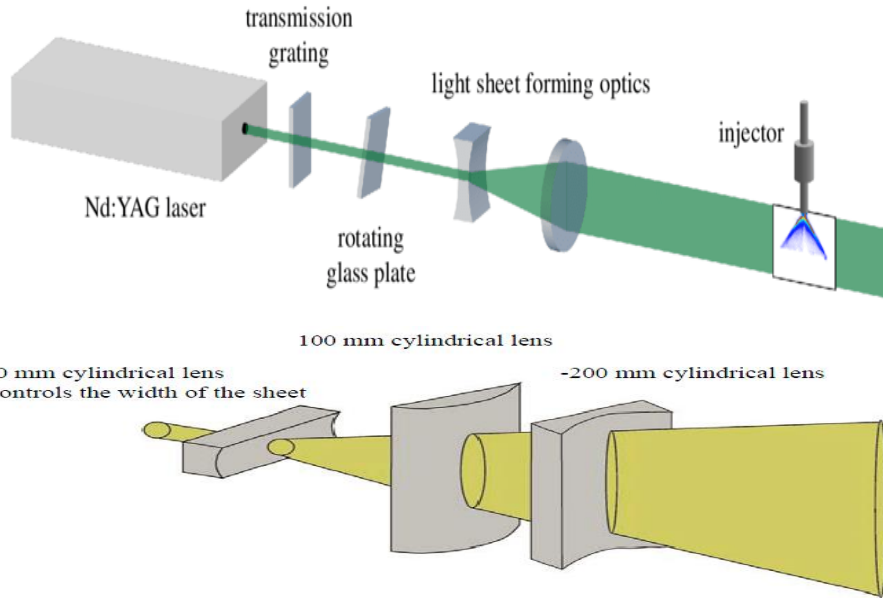
Figure 4-8: Gemini with Extended Base Plate for UV Operation



a.  $T=t_0$

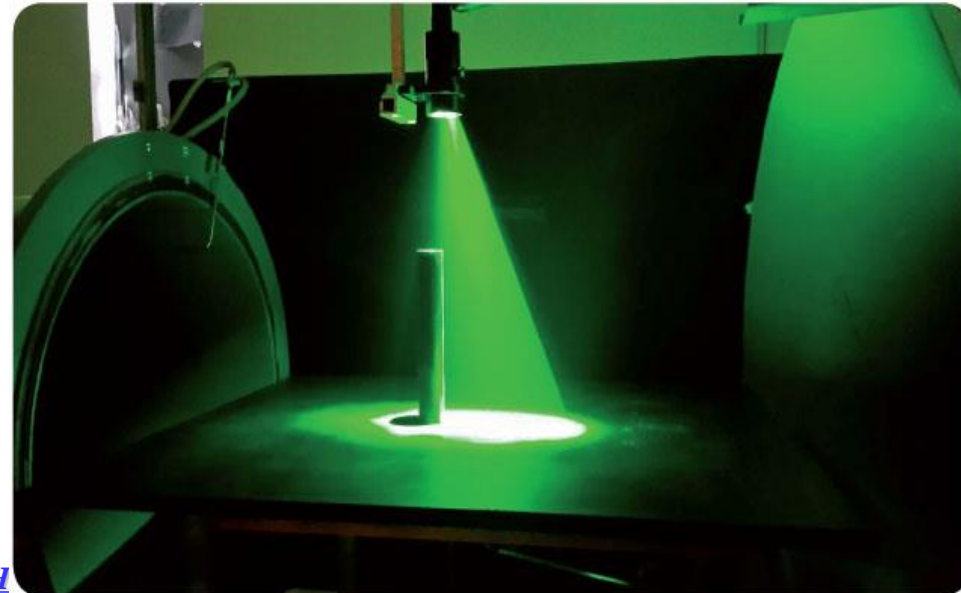
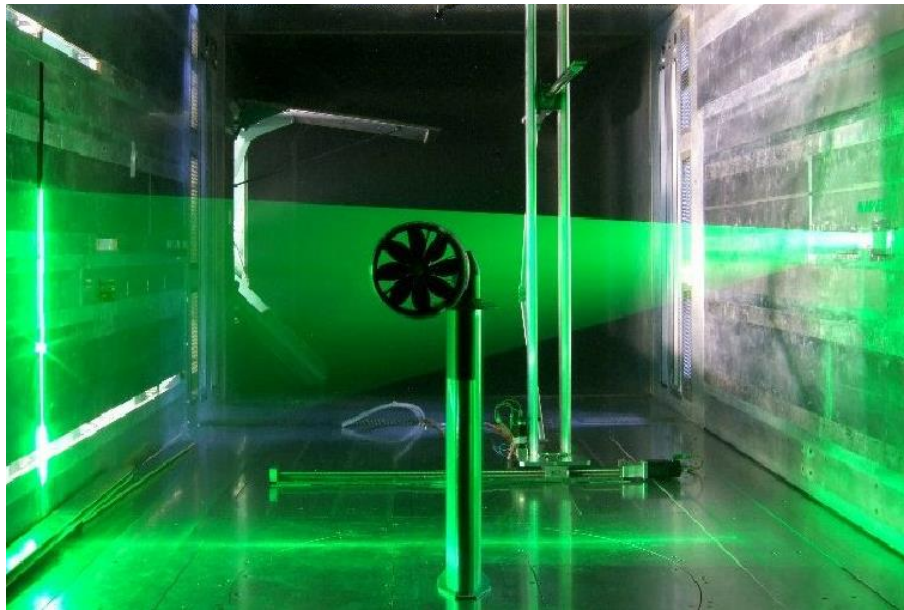
b.  $T=t_0+10\mu s$

# Optics/Lenses to shape Laser Beam to Sheet



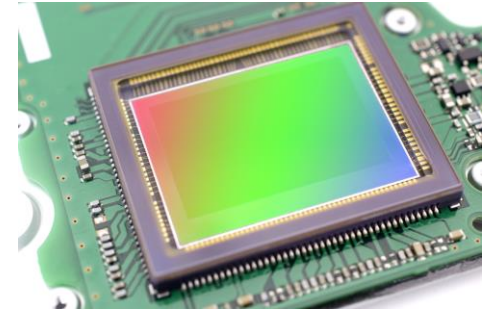
How Lenses Function

- <https://www.youtube.com/watch?v=EL9J3Km6wxI>



# Image Acquisition System: Cameras

- *The widely used cameras for PIV:*
  - *Photographic film-based cameras or digital cameras.*
- *Advantages of digital cameras:*
  - *It is fully digitized*
  - *Various digital techniques can be implemented for PIV image processing.*
  - *Conventional auto- or cross-correlation techniques combined with special framing techniques can be used to measure higher velocities.*
- *Disadvantages of digital cameras:*
  - *Low temporal resolution (defined by the video framing rate):*
  - *Low spatial resolution:*

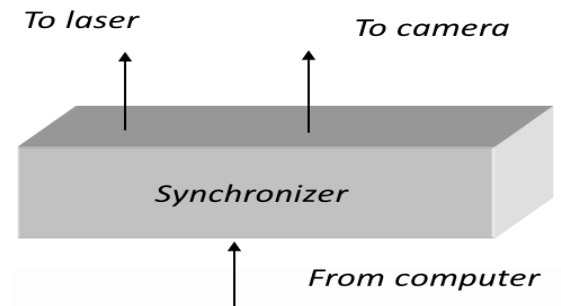
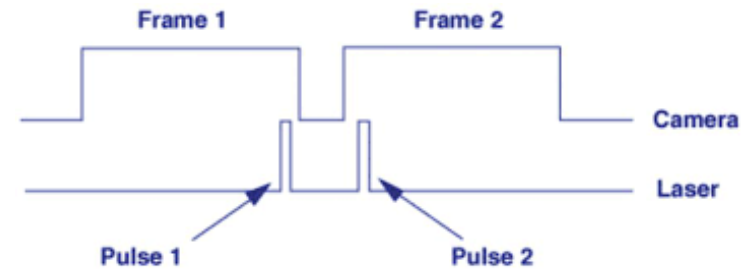
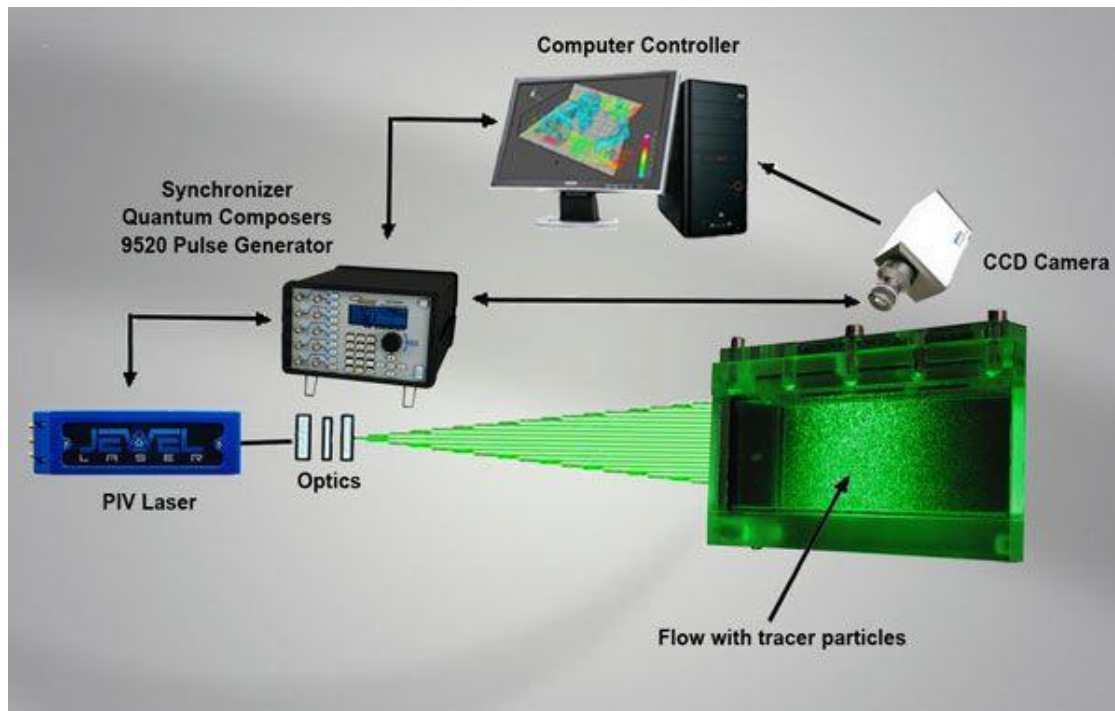


The Telegraph

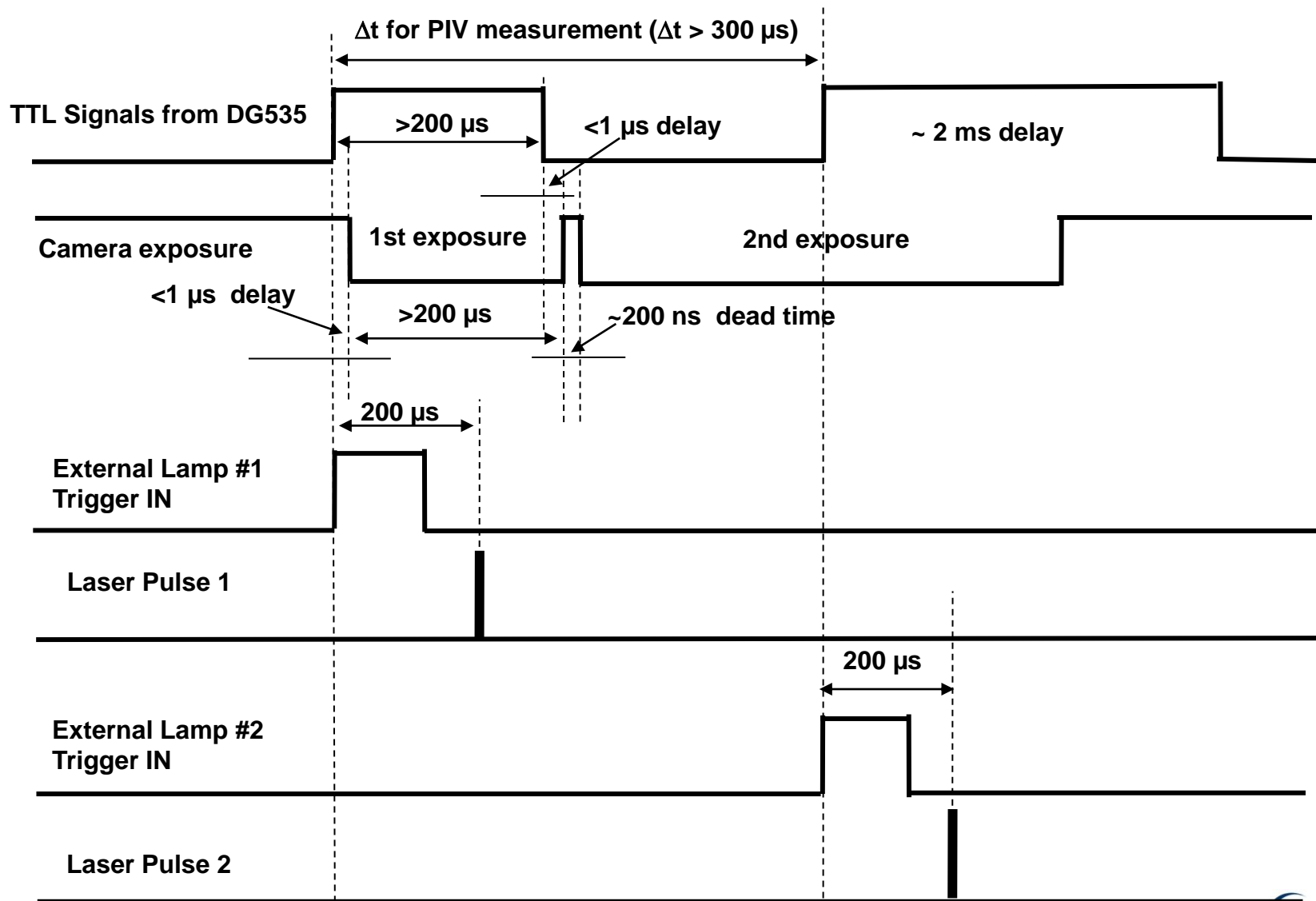
HOW A DIGITAL  
CAMERA WORKS

# Synchronizer

- **Function of Synchronizer:**
  - **To control the timing of the laser illumination and camera acquisition**

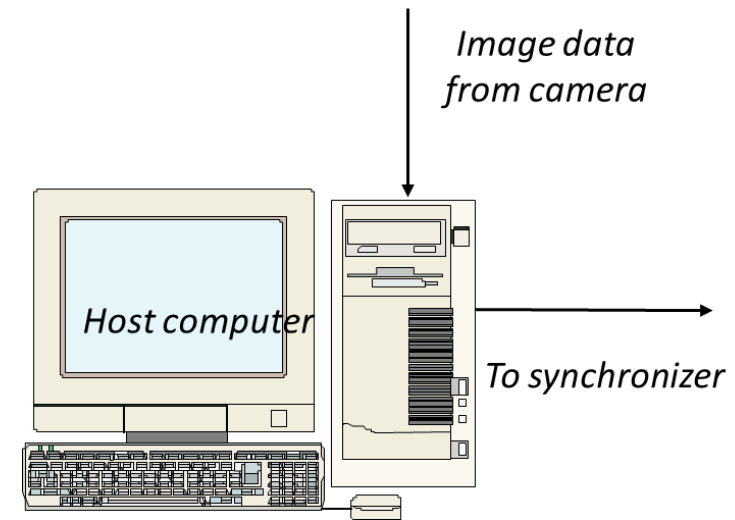
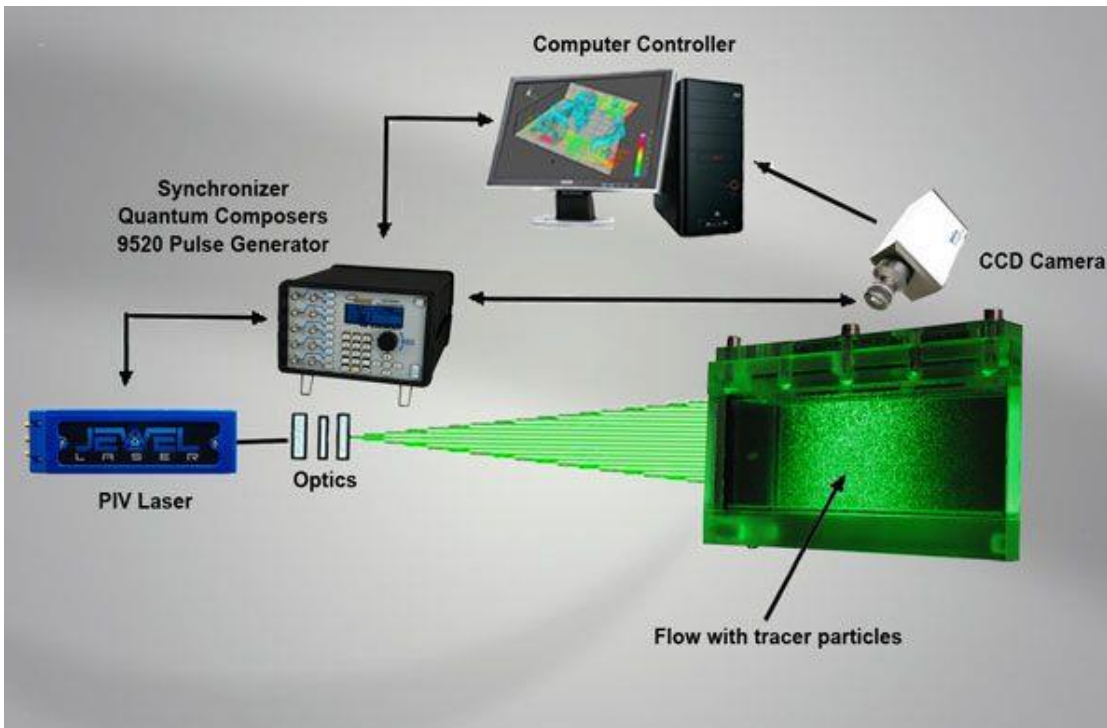


# Time Chart of the PIV Measurements ( $\Delta t > 300 \mu\text{s}$ )



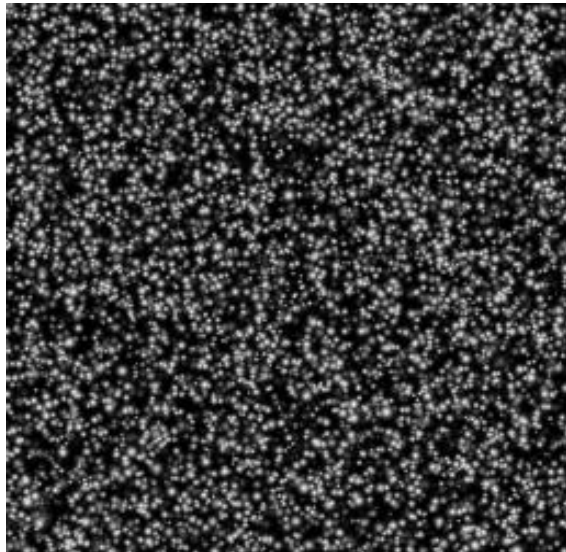
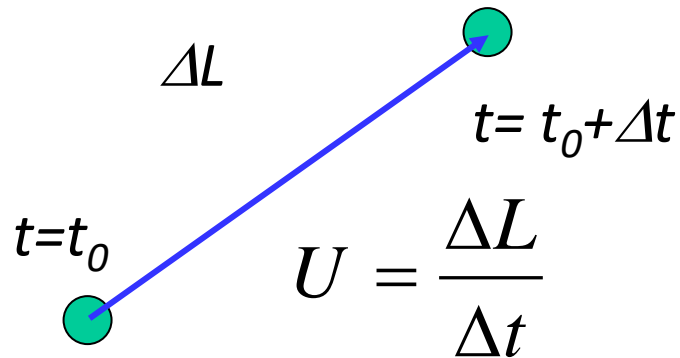
# Host computer

- *To send timing control parameter to synchronizer.*
- *To store the particle images and conduct image processing.*

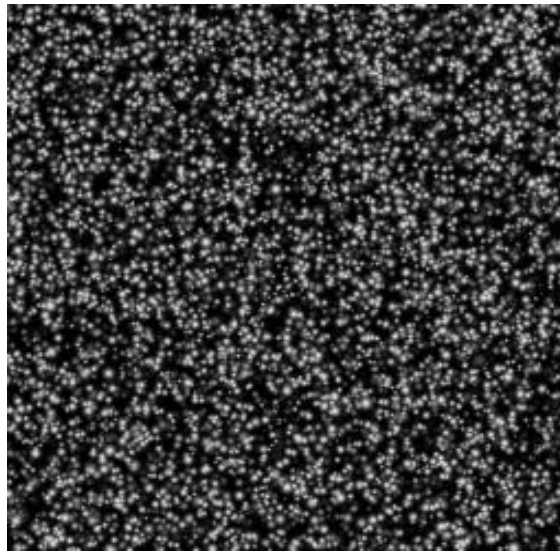


# PIV image Processing

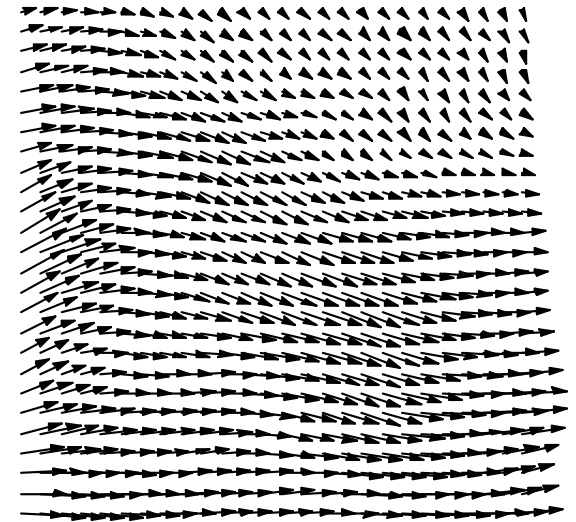
- Time-of-flight method: to measure the displacements of the tracer particles seeded in the flow in a fixed time interval.*



*a.  $T=t_0$*

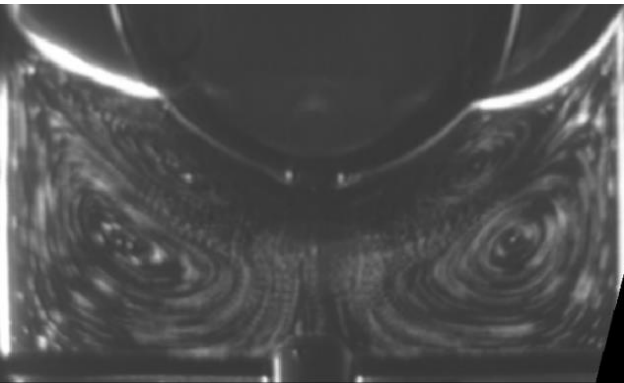
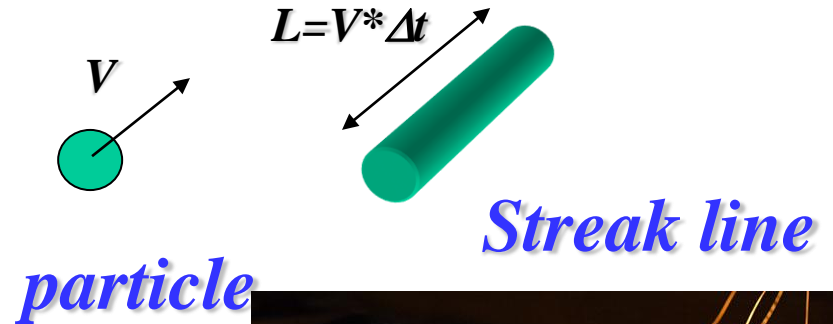
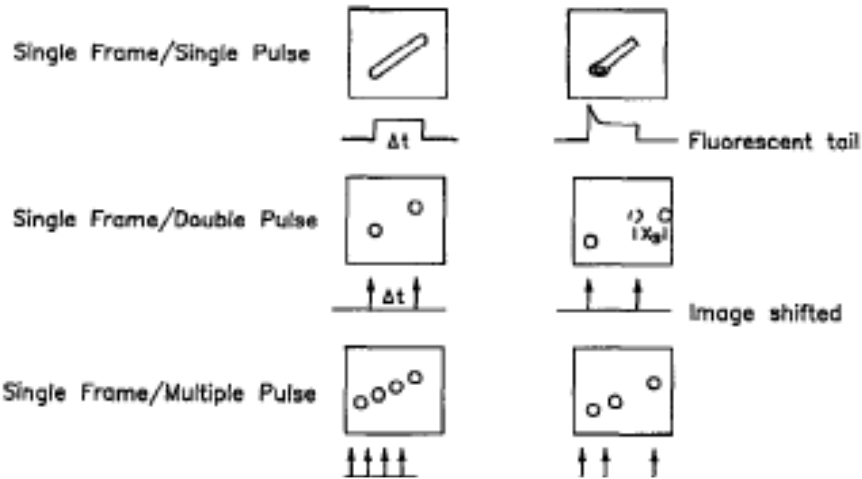


*b.  $T=t_0+4ms$*

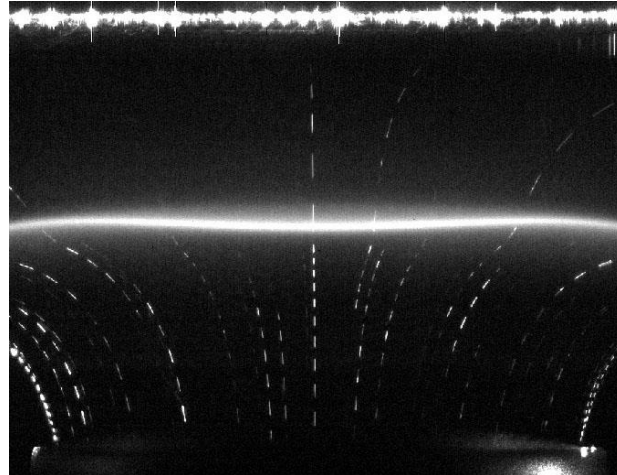


*Corresponding Velocity field*

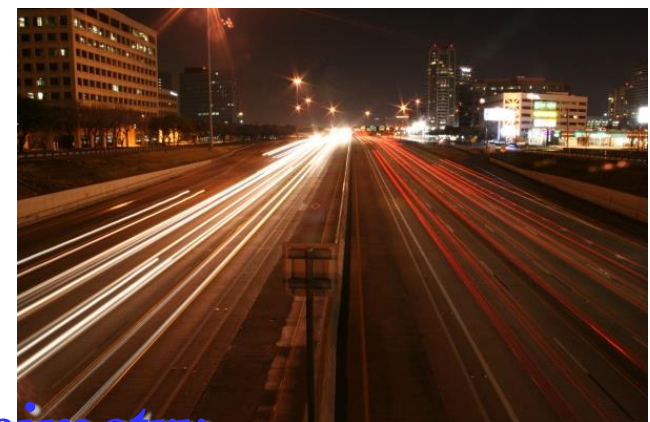
# Single-frame technique



*single-pulse*



*Multiple-pulse*





# Multi-frame technique

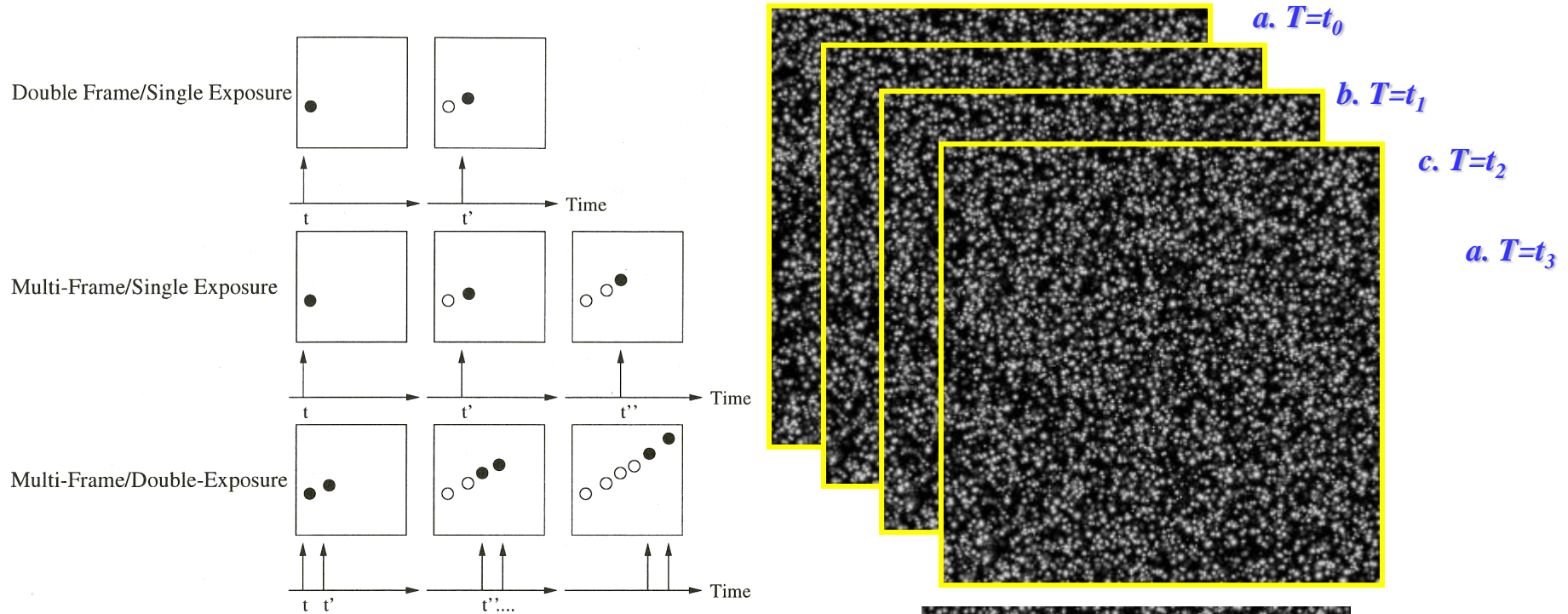
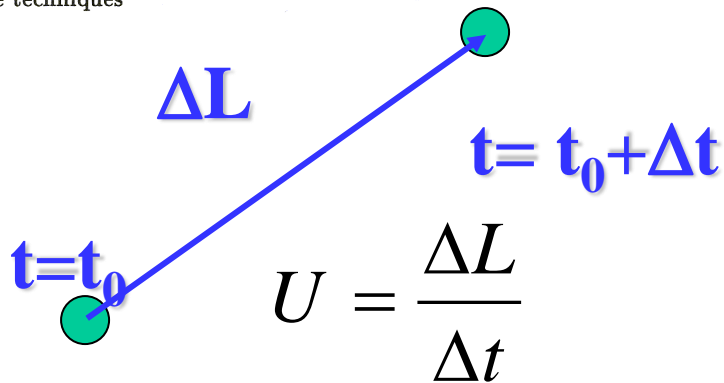
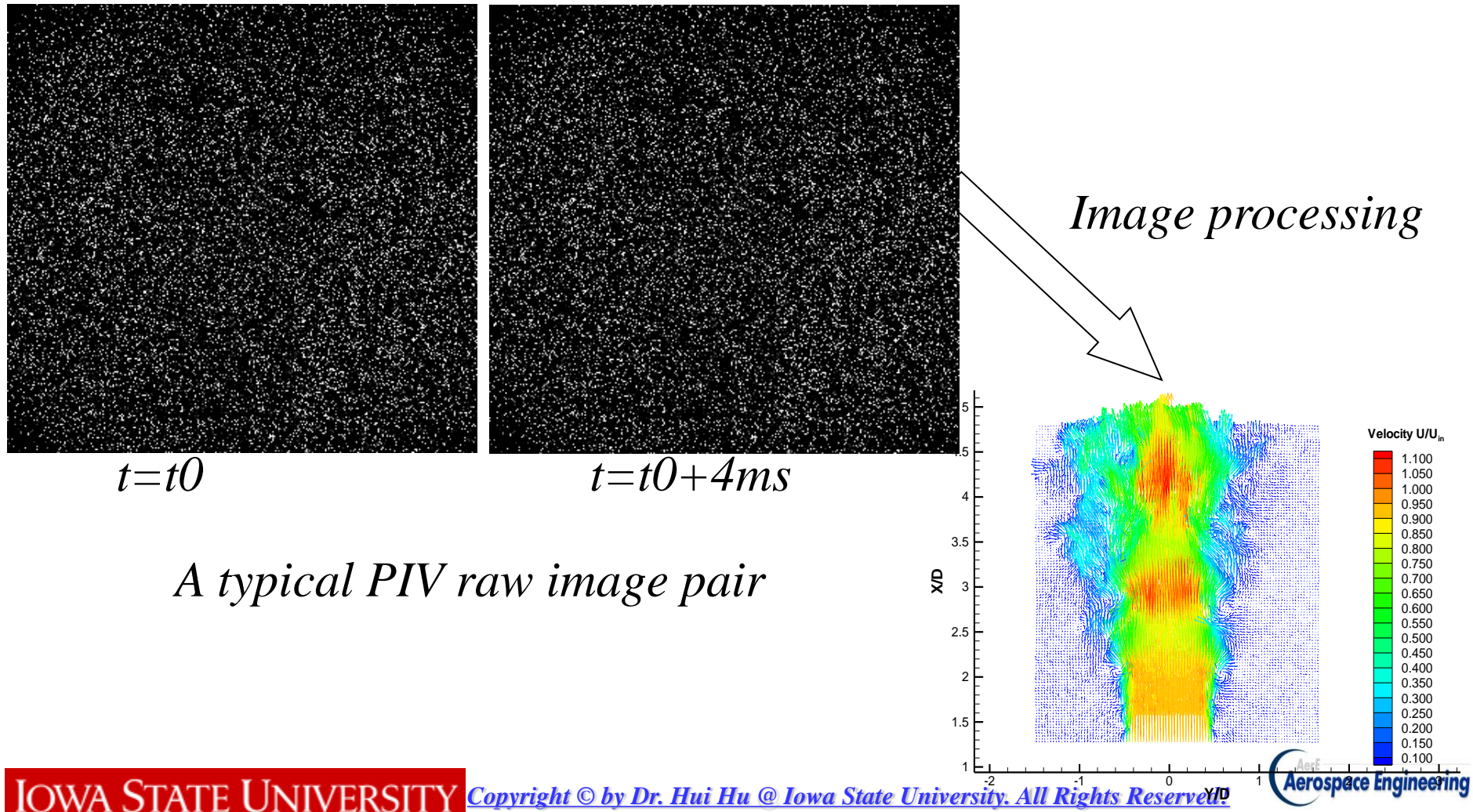


Fig. 4.2. Multiple frame techniques



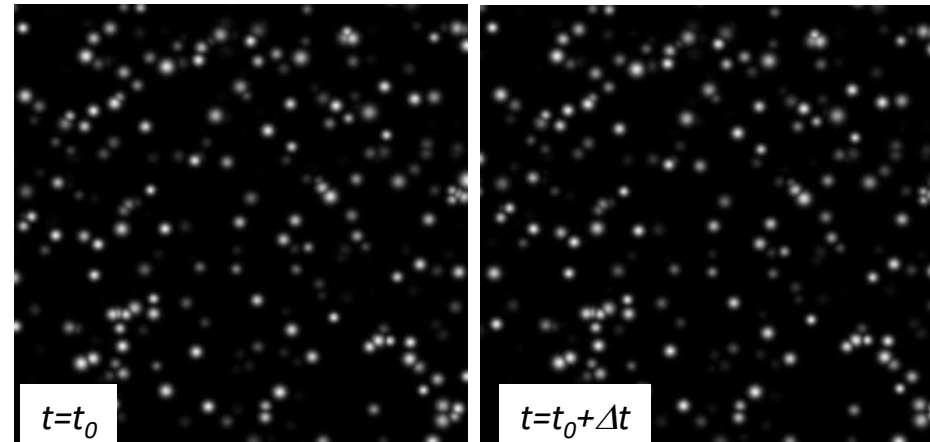
# Image Processing for PIV

- *To extract velocity information from particle images.*



# Particle Tracking Velocimetry (PTV)

1. Find position of the particles at each images
2. Find corresponding particle image pair in the different image frame
3. Find the displacements between the particle pairs.
4. Velocity of particle equates the displacement divided by the time interval between the frames.



*Low particle-image density case*

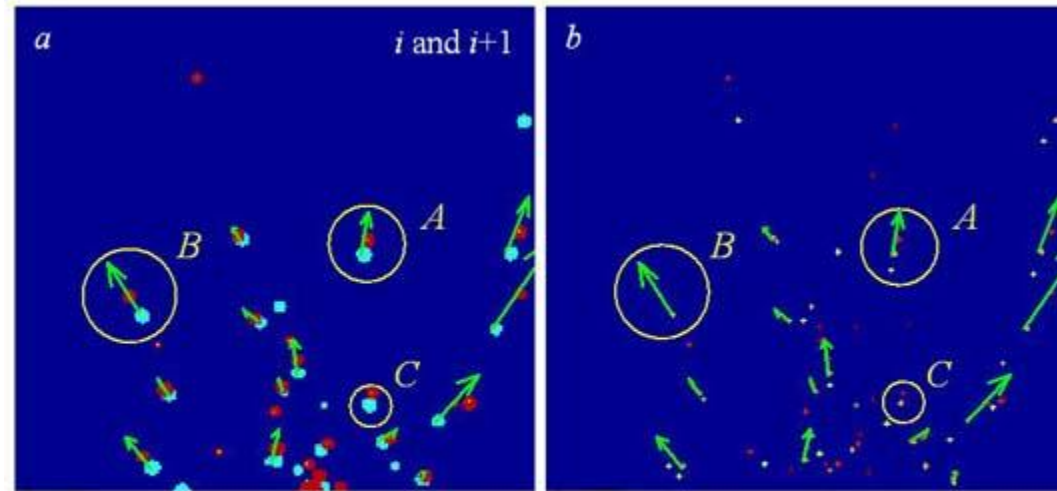
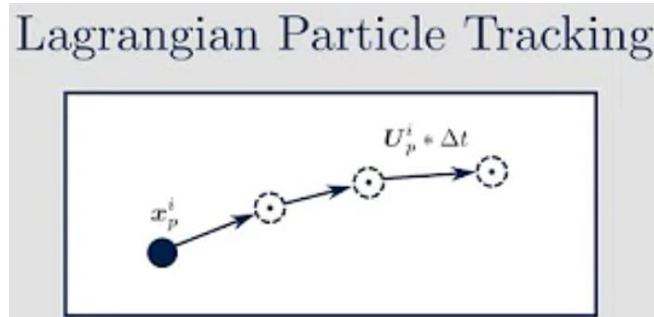
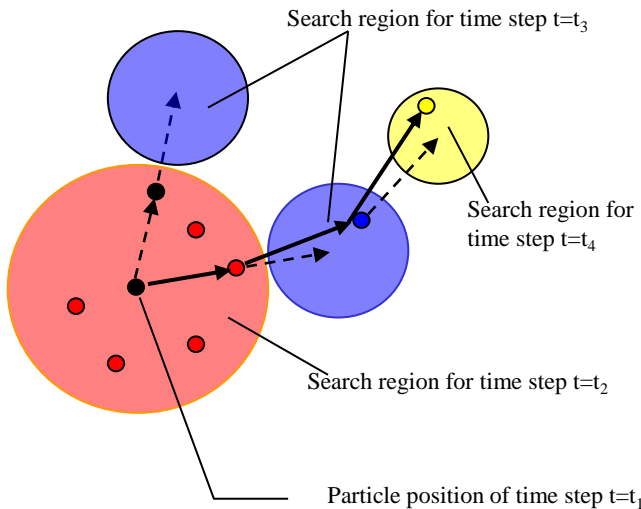
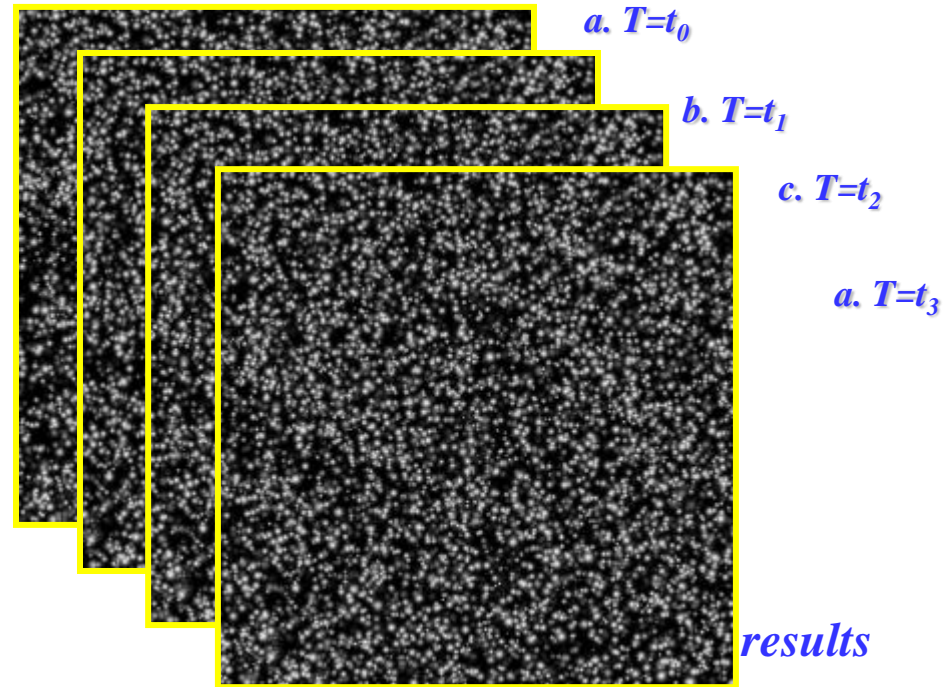


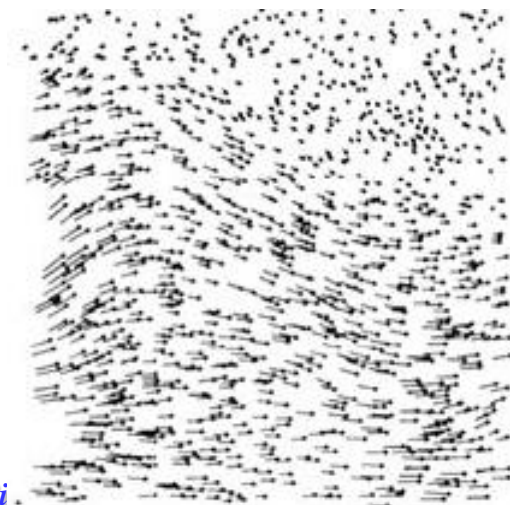
Figure 2. The particle-tracking algorithm applied to the sequence of images ( $i-1$ ) to ( $i+2$ ). (a) Detected particles in frames ( $i$ ) (light blue) and ( $i+1$ ) (dark red) with overlapped centroids and velocity vectors. (b) Detected centroids of particles in all four frames with overlaid velocity vectors. Consecutive frames are colored from light to dark.

# Particle Tracking Velocimetry (PTV)-2

1. Find position of the particles at each images
2. Find corresponding particle image pair in the different image frame
3. Find the displacements between the particle pairs.
4. Velocity of particle equates the displacement divided by the time interval between the frames.

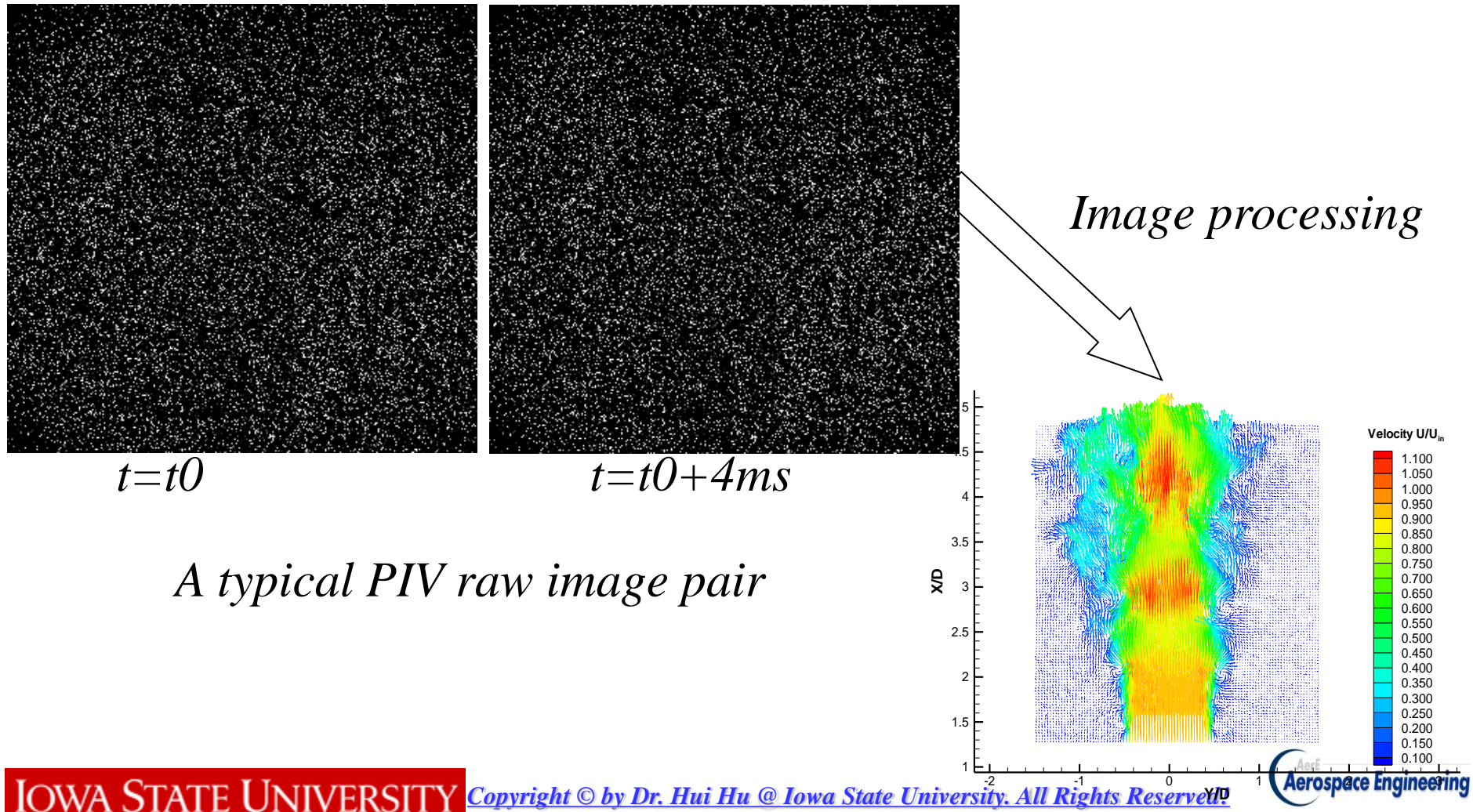


- **Four-frame-particle tracking algorithm**

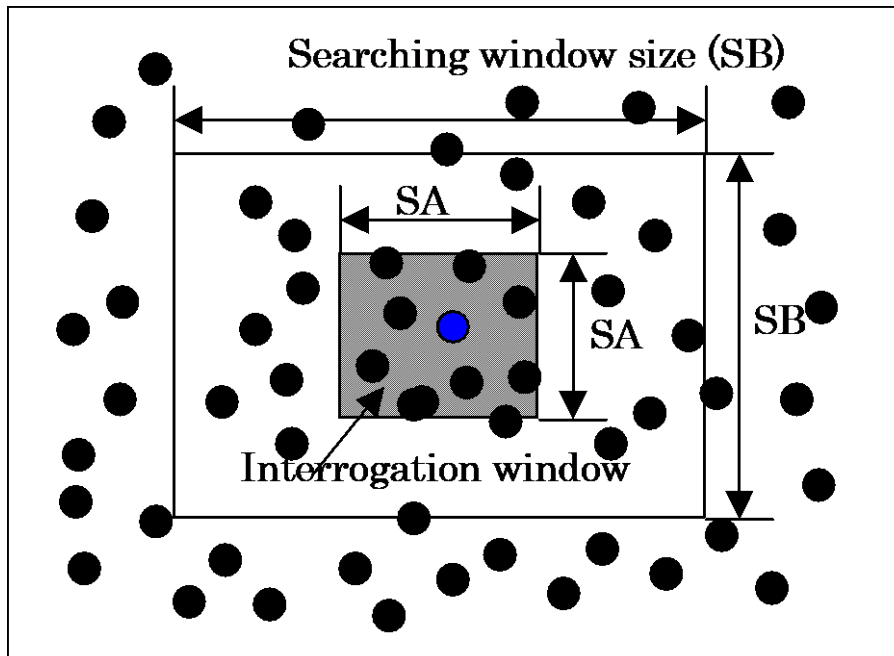


# Image Processing for PIV

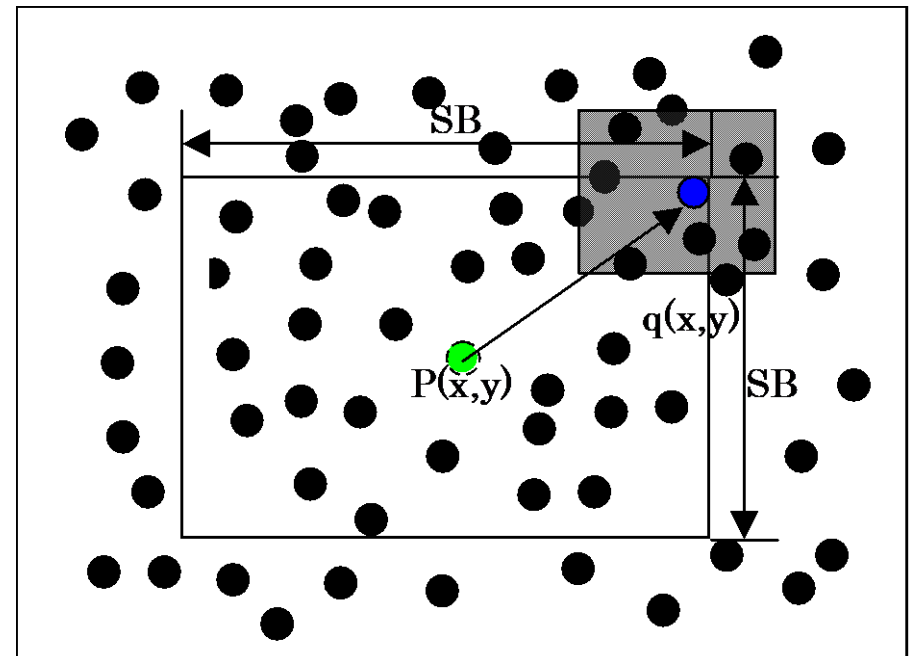
- *To extract velocity information from particle images.*



# Correlation-based PIV methods



$t=t_0$



$t=t_0 + \Delta t$

Correlation coefficient  
function

$$R(p, q) = \frac{\int (f(x, y) - \bar{f})(g(x, y) - \bar{g}) dv}{\sqrt{\int (f(x, y) - \bar{f})^2 dv \int (g(x, y) - \bar{g})^2 dv}}$$

# Cross Correlation Operation

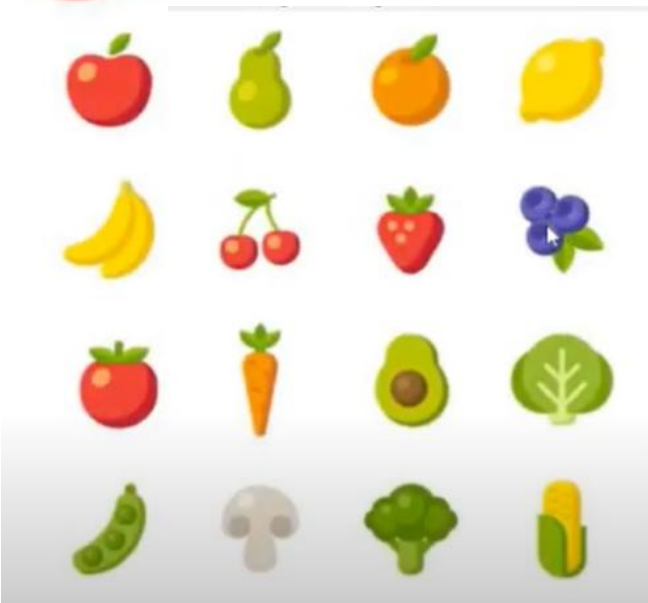


<https://www.youtube.com/watch?v=cbZUnuyxcVs>

## Pattern recognition



$$R(p,q) = \frac{\int (f(x,y) - \bar{f})(g(x,y) - \bar{g}) dv}{\sqrt{\int (f(x,y) - \bar{f})^2 dv \int (g(x,y) - \bar{g})^2 dv}}$$

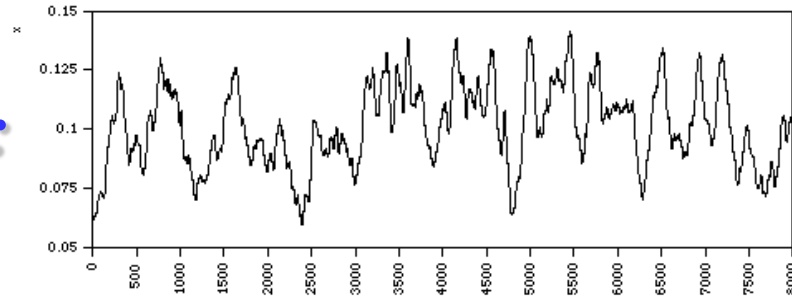


```
1 clc
2 clear all
3 close all
4 a=imread('Capture1.JPG');
5 at=rgb2gray(a);
6 figure;
7 imshow(a);
8 title('Original Image');
9 bt=imread('Capture2.JPG');
10 b=rgb2gray(bt);
11 figure;
12 imshow(bt);
13 title('Pattern');
14 cross=normxcorr2(b,at);
15 [y x]=find(cross>=0.86*max(cross(:)));
16 ynew=y-size(b,1);
17 xnew=x-size(b,2);
18 figure;
```

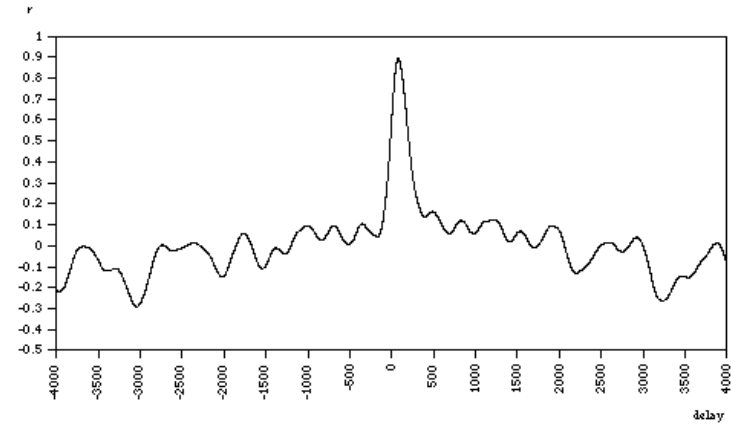
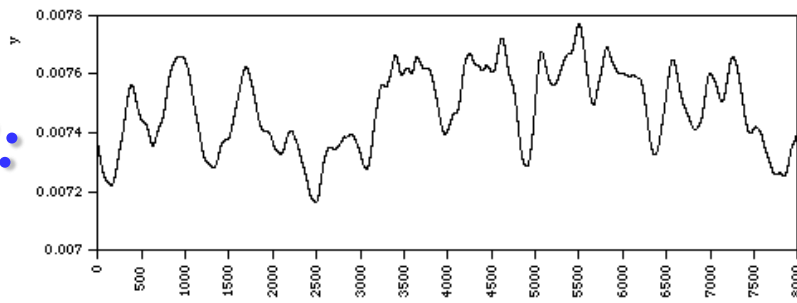
Hello.jpg OP... Command Window

# Cross Correlation Operation

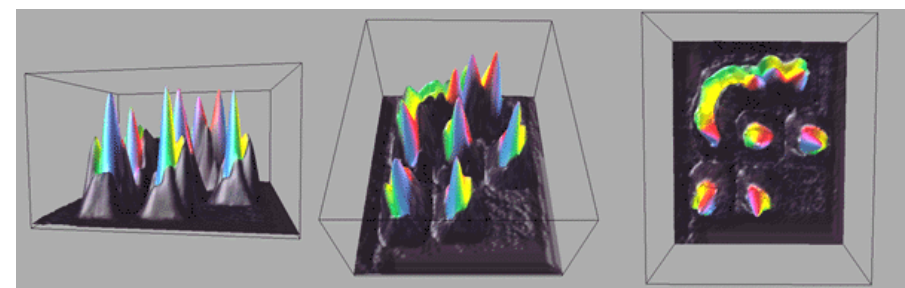
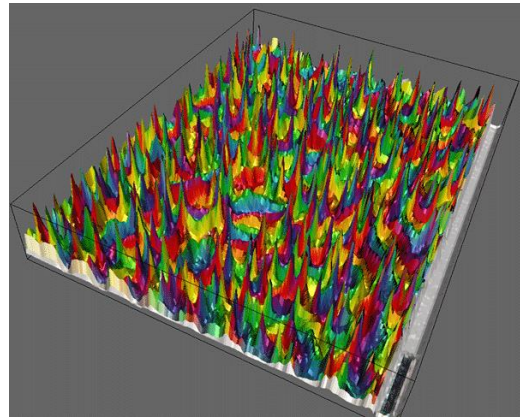
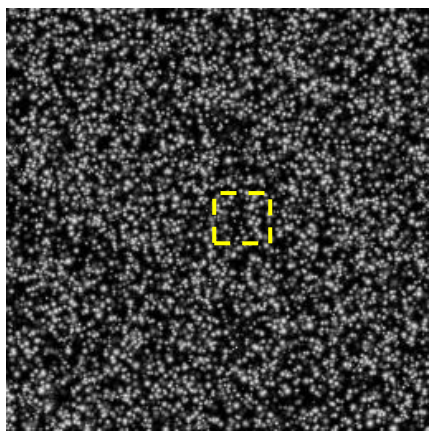
*Signal A:*



*Signal B:*



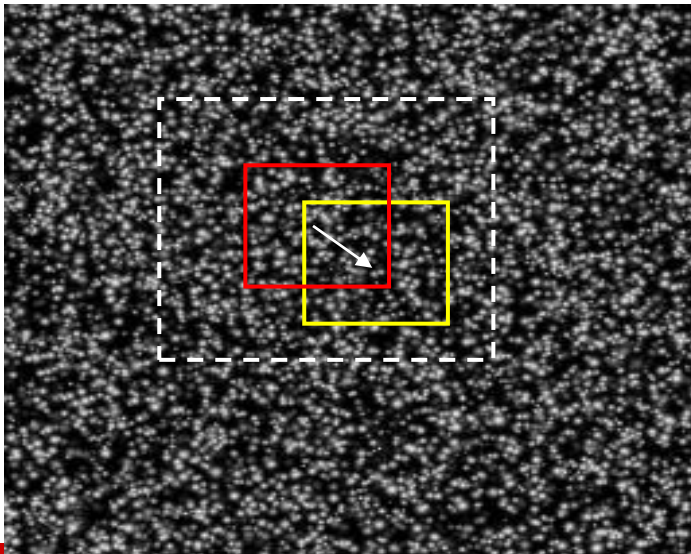
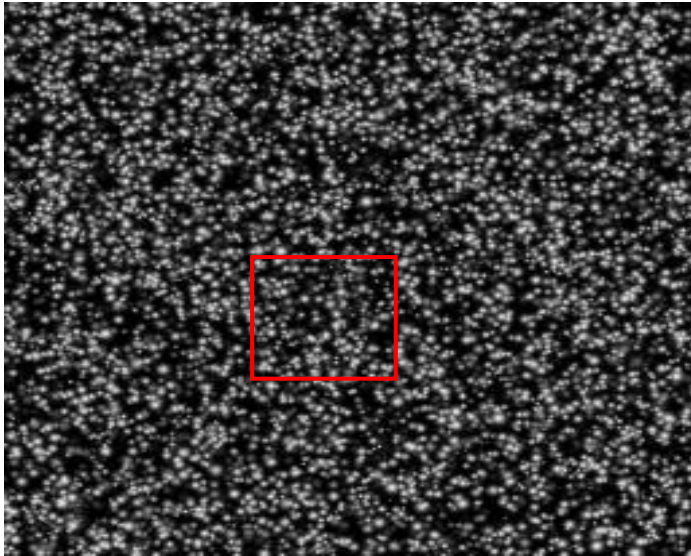
$$R(u) = \frac{\int [f(x) * g(x+u)] dx}{\sqrt{\int [f(x)^2] dx * \int [g(x+u)^2] dx}}$$



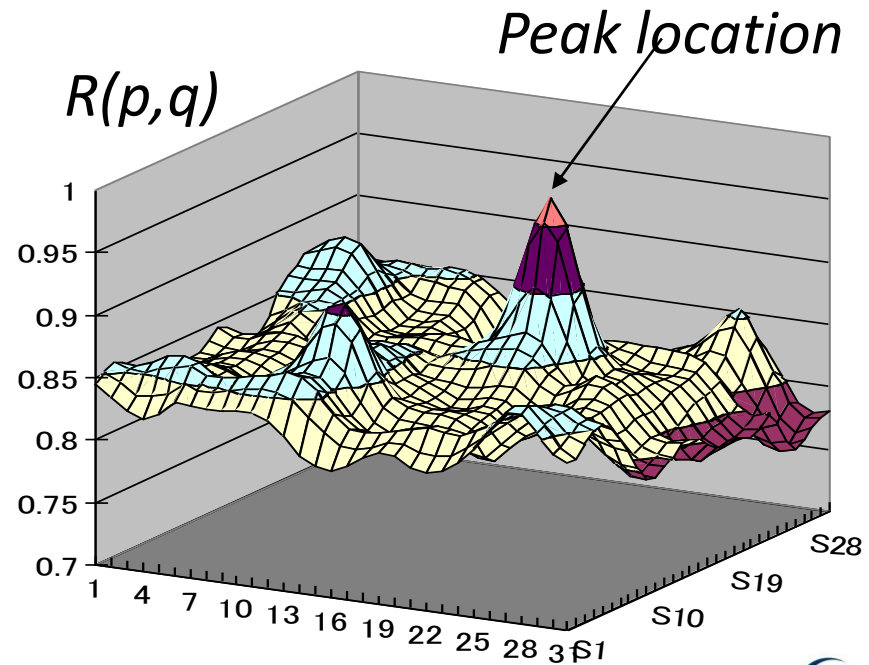
$$c(u, v) = \sum_{x, y} f(x, y) t(x - u, y - v)$$



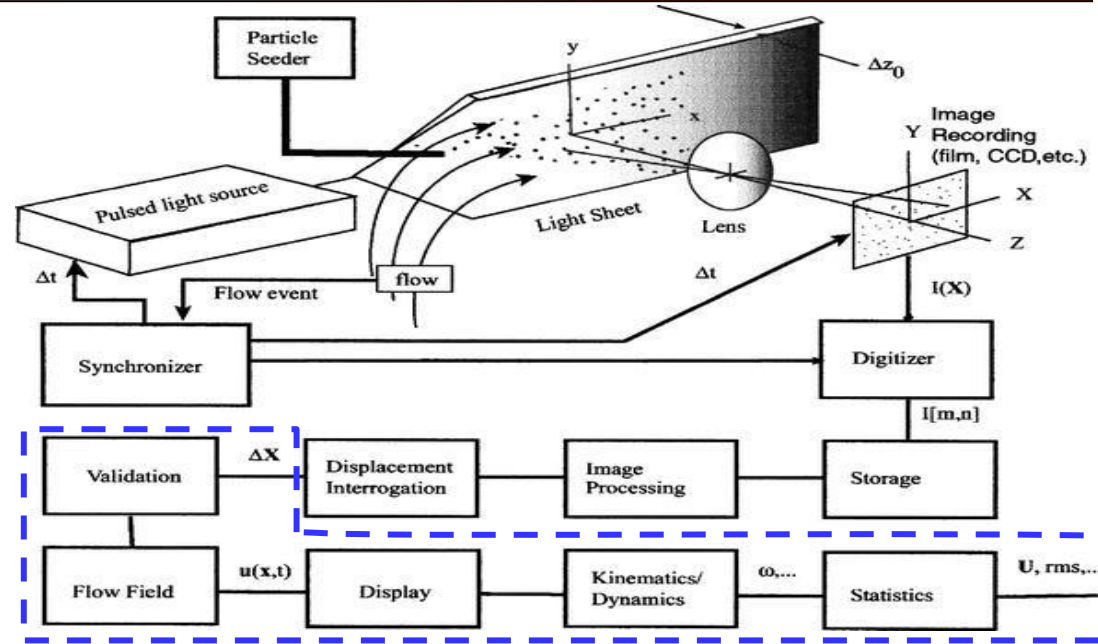
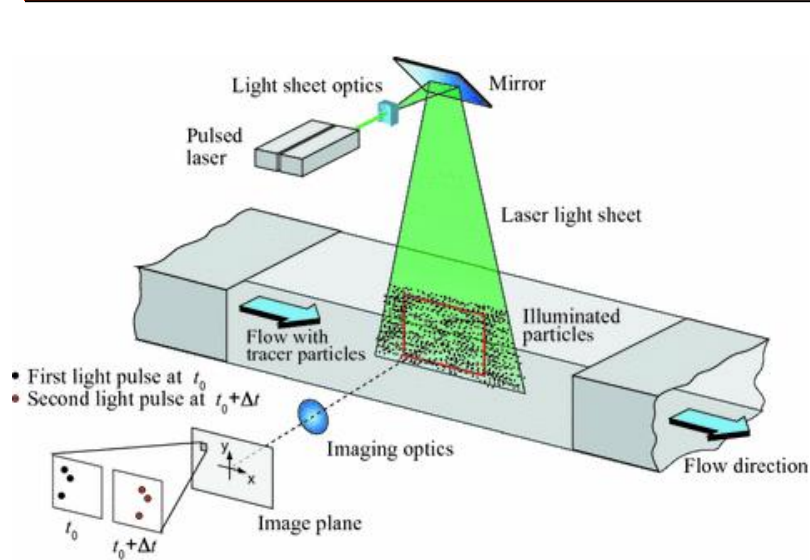
# CORRELATION COEFFICIENT DISTRIBUTION



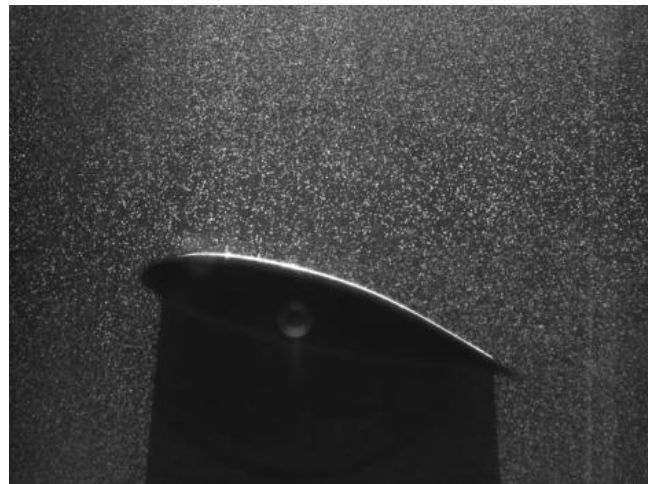
$$R(p, q) = \frac{\int (f(x, y) - \bar{f})(g(x, y) - \bar{g}) dv}{\sqrt{\int (f(x, y) - \bar{f})^2 dv \int (g(x, y) - \bar{g})^2 dv}}$$



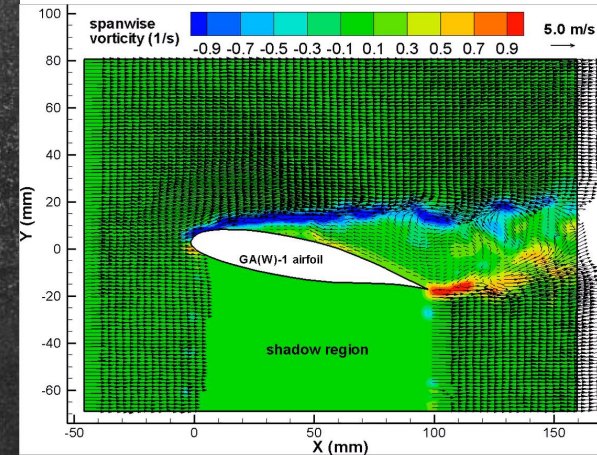
# Post processing of PIV measurements



a.  $T=t_0$



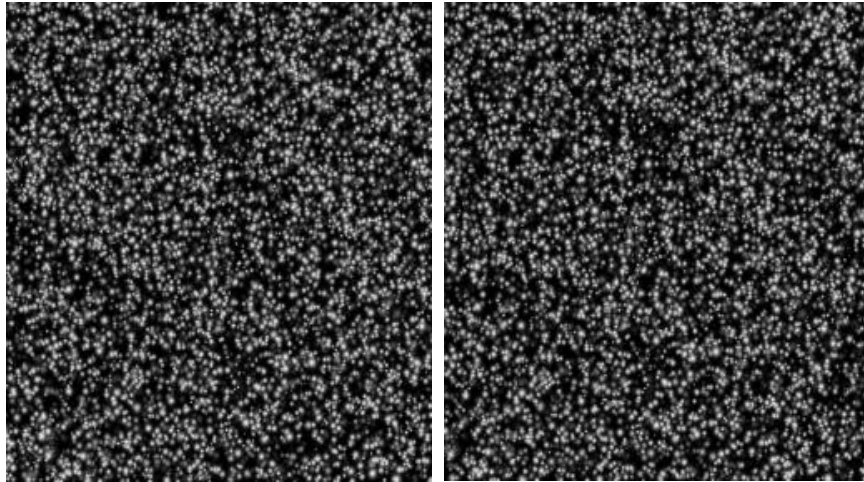
b.  $T=t_0+10\mu s$



Corresponding Velocity field

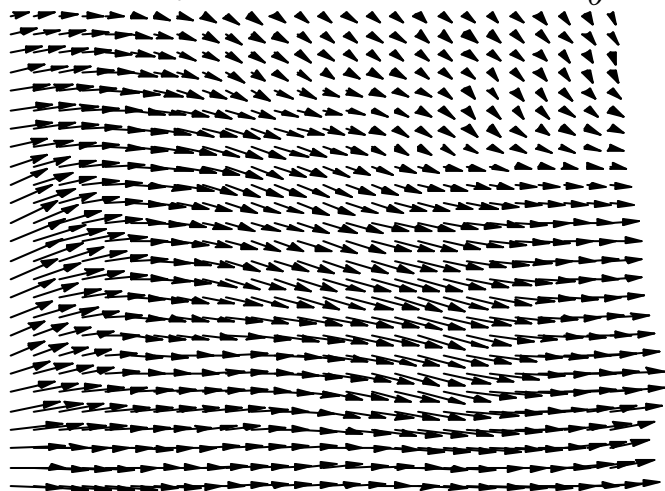
# Post processing: Detection of spurious vectors

- *Ideal case*



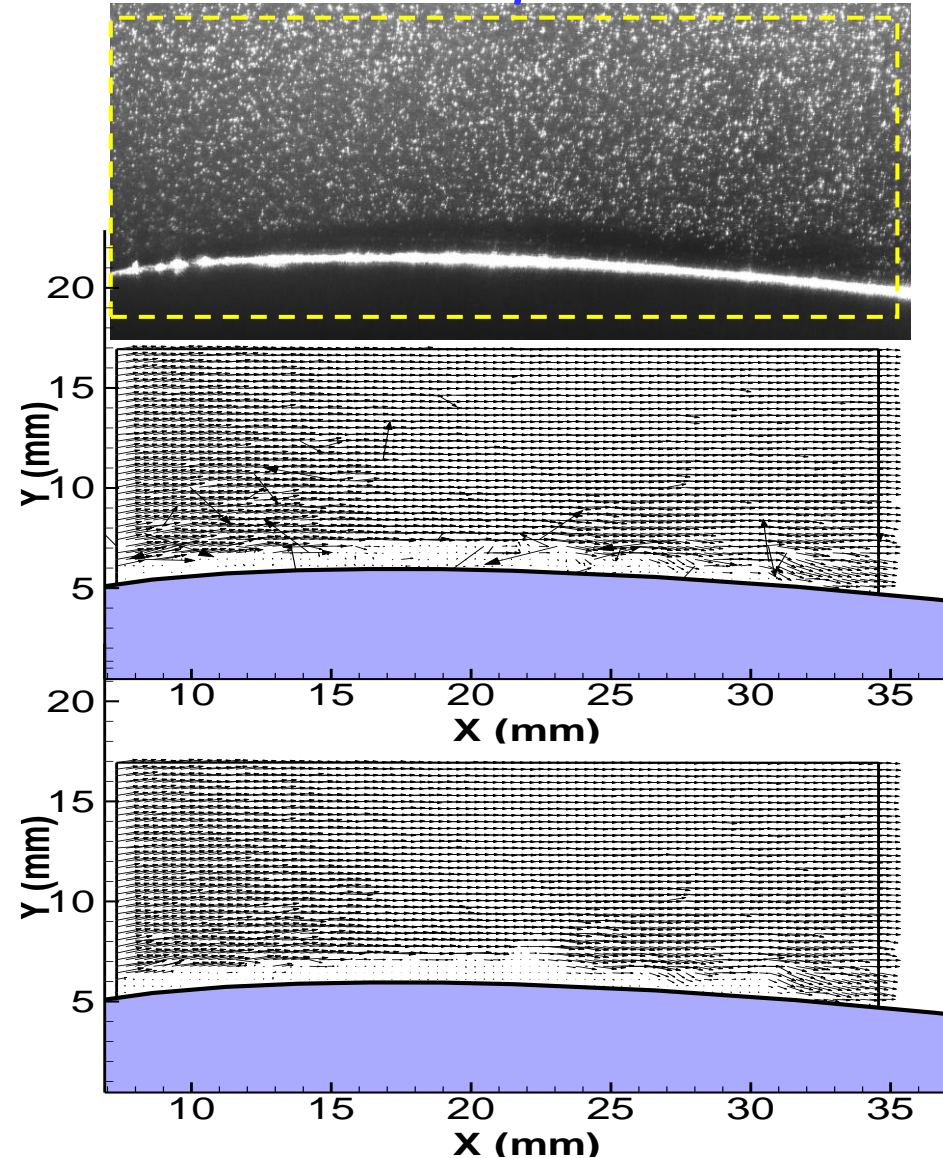
*a.  $t = t_0$*

*b.  $t = t_0 + \Delta t$*

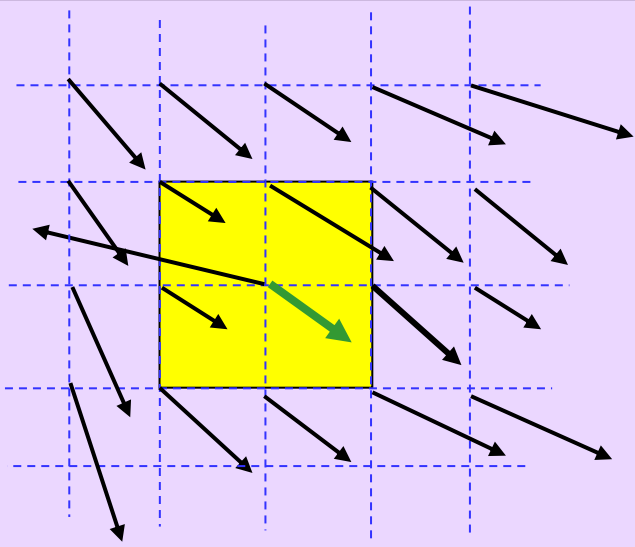


Corresponding flow velocity field

- *Real experiment*



# Detection of spurious vectors



$$Um = \frac{U_{i+1,j-1} + U_{i+1,j} + U_{i+1,j+1} + U_{i,j-1} + U_{i,j+1} + U_{i-1,j-1} + U_{i-1,j} + U_{i-1,j+1}}{8}$$

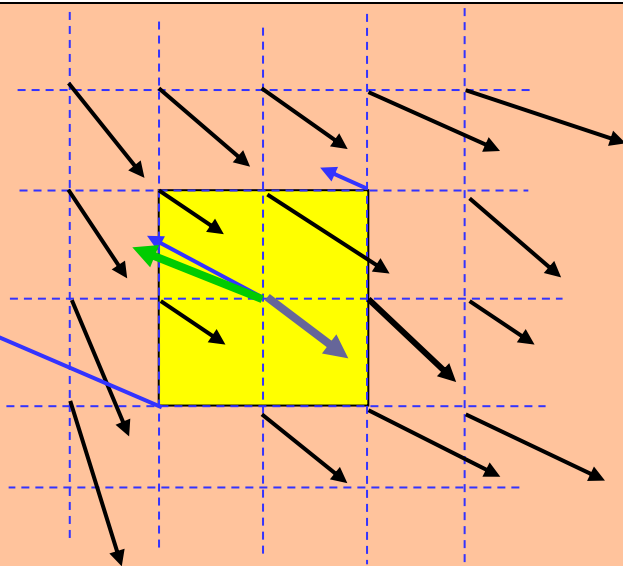
$$Vm = \frac{V_{i+1,j-1} + V_{i+1,j} + V_{i+1,j+1} + V_{i,j-1} + V_{i,j+1} + V_{i-1,j-1} + V_{i-1,j} + V_{i-1,j+1}}{8}$$

$$R\_value = \frac{\sqrt{(U_{i,j} - Um)^2 + (V_{i,j} - Vm)^2}}{\sqrt{Um^2 + Vm^2}} \approx \frac{\sqrt{(U_{i,j} - Um)^2 + (V_{i,j} - Vm)^2}}{\sqrt{Um^2 + Vm^2} + \varepsilon}$$

$\varepsilon$ : is a very small number, such as 0.000000001.

$R\_value > R_{thresh\_hold}$  for a spurious vector

- **Regular method**



$$Um = \frac{U_{i+1,j-1} + U_{i+1,j} + U_{i+1,j+1} + U_{i,j-1} + U_{i,j+1} + U_{i-1,j-1} + U_{i-1,j} + U_{i-1,j+1} - U_{max} - U_{min}}{6}$$

$$Vm = \frac{V_{i+1,j-1} + V_{i+1,j} + V_{i+1,j+1} + V_{i,j-1} + V_{i,j+1} + V_{i-1,j-1} + V_{i-1,j} + V_{i-1,j+1} - V_{max} - V_{min}}{6}$$

$$R\_value = \frac{\sqrt{(U_{i,j} - Um)^2 + (V_{i,j} - Vm)^2}}{\sqrt{Um^2 + Vm^2}} \approx \frac{\sqrt{(U_{i,j} - Um)^2 + (V_{i,j} - Vm)^2}}{\sqrt{Um^2 + Vm^2} + \varepsilon}$$

$\varepsilon$ : is a very small number, such as 0.000000001.

$R\_value > R_{thresh\_hold}$  for a spurious vector

- **Median test method**

# Estimation of differential quantities

$$\frac{d\mathbf{U}}{d\mathbf{X}} = \begin{bmatrix} \frac{\partial U}{\partial X} & \frac{\partial V}{\partial X} & \frac{\partial W}{\partial X} \\ \frac{\partial U}{\partial Y} & \frac{\partial V}{\partial Y} & \frac{\partial W}{\partial Y} \\ \frac{\partial U}{\partial Z} & \frac{\partial V}{\partial Z} & \frac{\partial W}{\partial Z} \end{bmatrix} \quad (6.7)$$

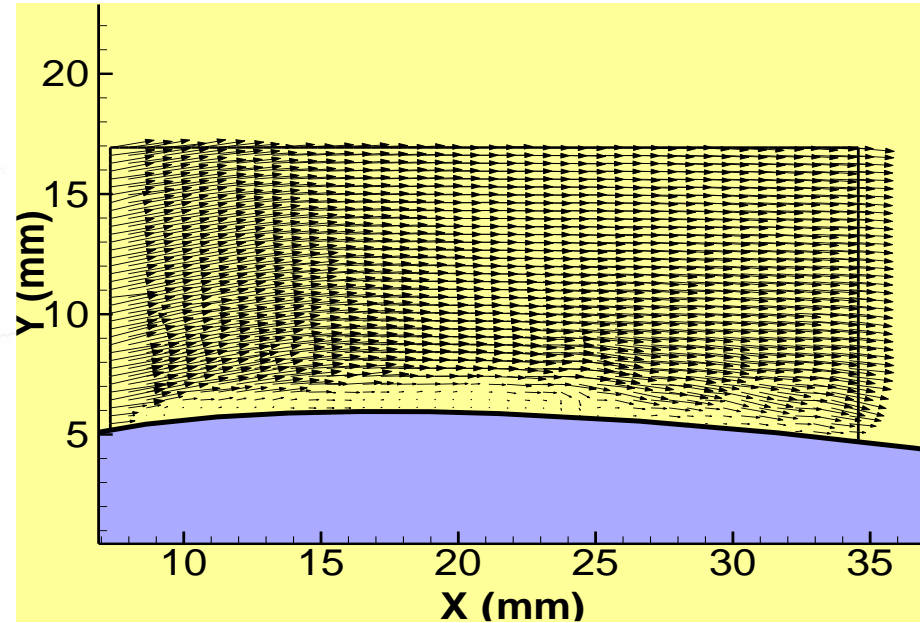
This deformation tensor can be decomposed into a symmetric part and an antisymmetric part:

$$\frac{d\mathbf{U}}{d\mathbf{X}} = \begin{bmatrix} \frac{\partial U}{\partial X} & \frac{1}{2}(\frac{\partial V}{\partial X} + \frac{\partial U}{\partial Y}) & \frac{1}{2}(\frac{\partial W}{\partial X} + \frac{\partial U}{\partial Z}) \\ \frac{1}{2}(\frac{\partial U}{\partial Y} + \frac{\partial V}{\partial X}) & \frac{\partial V}{\partial Y} & \frac{1}{2}(\frac{\partial W}{\partial Y} + \frac{\partial V}{\partial Z}) \\ \frac{1}{2}(\frac{\partial U}{\partial Z} + \frac{\partial W}{\partial X}) & \frac{1}{2}(\frac{\partial V}{\partial Z} + \frac{\partial W}{\partial Y}) & \frac{\partial W}{\partial Z} \end{bmatrix} \quad (6.8)$$

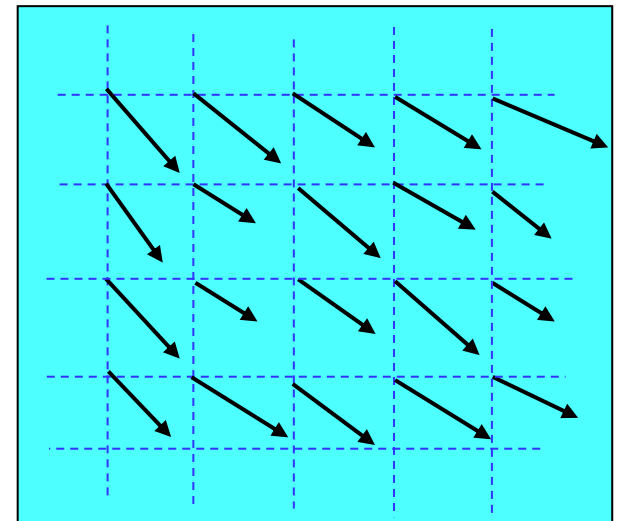
$$+ \begin{bmatrix} 0 & \frac{1}{2}(\frac{\partial V}{\partial X} - \frac{\partial U}{\partial Y}) & \frac{1}{2}(\frac{\partial W}{\partial X} - \frac{\partial U}{\partial Z}) \\ \frac{1}{2}(\frac{\partial U}{\partial Y} - \frac{\partial V}{\partial X}) & 0 & \frac{1}{2}(\frac{\partial W}{\partial Y} - \frac{\partial V}{\partial Z}) \\ \frac{1}{2}(\frac{\partial U}{\partial Z} - \frac{\partial W}{\partial X}) & \frac{1}{2}(\frac{\partial V}{\partial Z} - \frac{\partial W}{\partial Y}) & 0 \end{bmatrix} \quad (6.9)$$

A substitution of the strain and vorticity components yields:

$$\frac{d\mathbf{U}}{d\mathbf{X}} = \begin{bmatrix} \epsilon_{XX} & \frac{1}{2}\epsilon_{XY} & \frac{1}{2}\epsilon_{XZ} \\ \frac{1}{2}\epsilon_{YX} & \epsilon_{YY} & \frac{1}{2}\epsilon_{YZ} \\ \frac{1}{2}\epsilon_{ZX} & \frac{1}{2}\epsilon_{ZY} & \epsilon_{ZZ} \end{bmatrix} + \begin{bmatrix} 0 & \frac{1}{2}\omega_Z & -\frac{1}{2}\omega_X \\ -\frac{1}{2}\omega_Z & 0 & \frac{1}{2}\omega_Y \\ -\frac{1}{2}\omega_X & \frac{1}{2}\omega_Y & 0 \end{bmatrix} \quad (6.10)$$

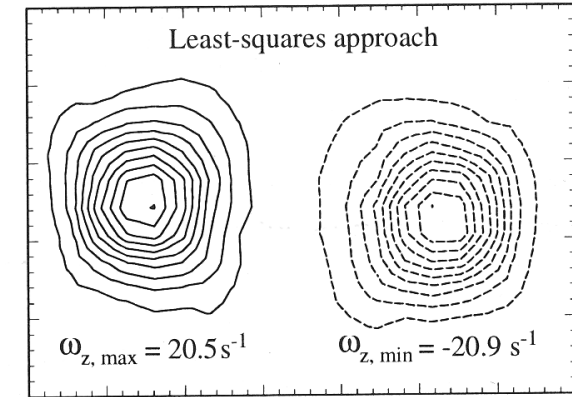
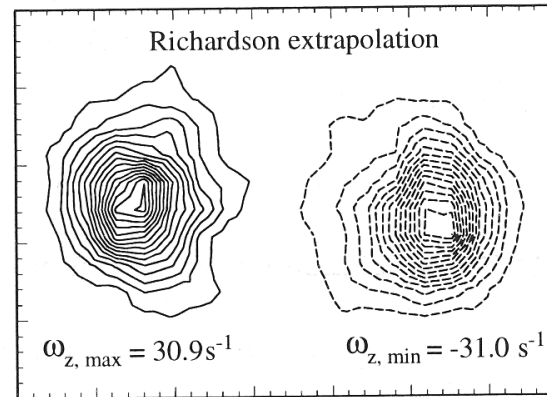
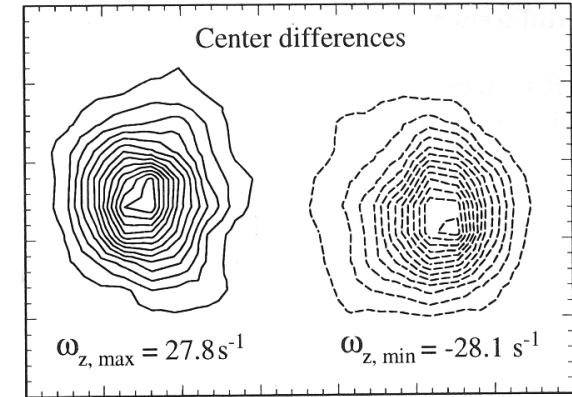
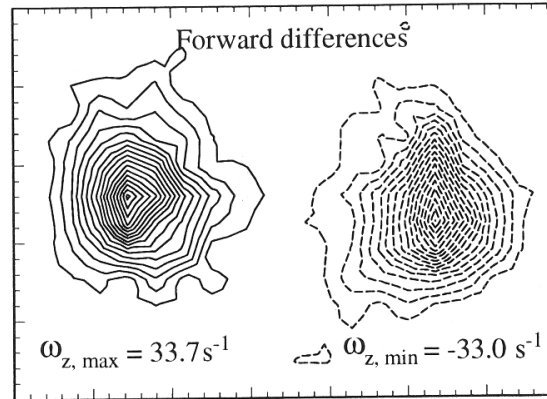
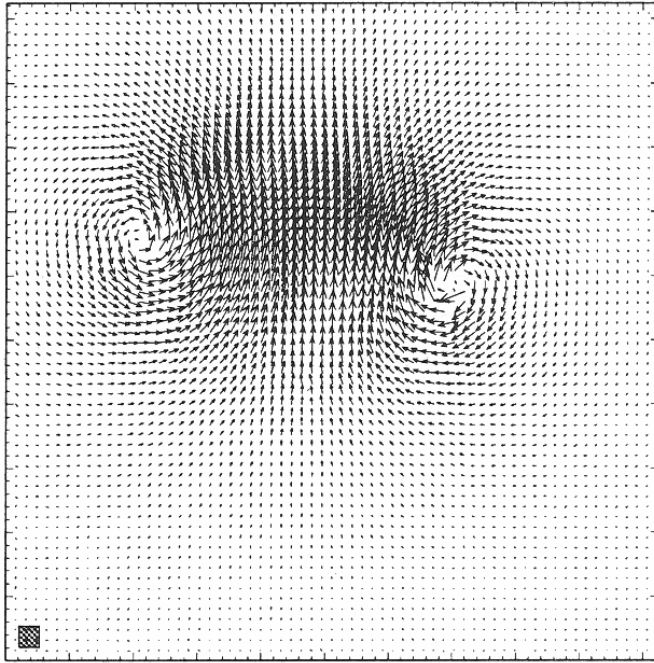


Operator	Implementation	Accuracy	Uncertainty
Forward difference	$\left(\frac{df}{dx}\right)_{i+1/2} \approx \frac{f_{i+1} - f_i}{\Delta X}$	$O(\Delta X)$	$\approx 1.41 \frac{\epsilon_U}{\Delta X}$
Backward difference	$\left(\frac{df}{dx}\right)_{i-1/2} \approx \frac{f_i - f_{i-1}}{\Delta X}$	$O(\Delta X)$	$\approx 1.41 \frac{\epsilon_U}{\Delta X}$
Center difference	$\left(\frac{df}{dx}\right)_i \approx \frac{f_{i+1} - f_{i-1}}{2\Delta X}$	$O(\Delta X^2)$	$\approx 0.7 \frac{\epsilon_U}{\Delta X}$
Richardson extrapol.	$\left(\frac{df}{dx}\right)_i \approx \frac{f_{i-2} - 8f_{i-1} + 8f_{i+1} - f_{i+2}}{12\Delta X}$	$O(\Delta X^3)$	$\approx 0.95 \frac{\epsilon_U}{\Delta X}$
Least squares	$\left(\frac{df}{dx}\right)_i \approx \frac{2f_{i+2} + f_{i+1} - f_{i-1} - 2f_{i-2}}{10\Delta X}$	$O(\Delta X^2)$	$\approx 1.0 \frac{\epsilon_U}{\Delta X}$



# Estimation of Vorticity distribution

$$\omega_z = \frac{\partial V}{\partial x} - \frac{\partial U}{\partial y}$$



**Fig. 6.7.** Vorticity field estimates obtained from twice oversampled PIV data, e.g. the interrogation window overlap is 50%. The vortex pair is known to be laminar and thus should have smooth vorticity contours

# Estimation of Vorticity distribution

- Stokes Theorem:**

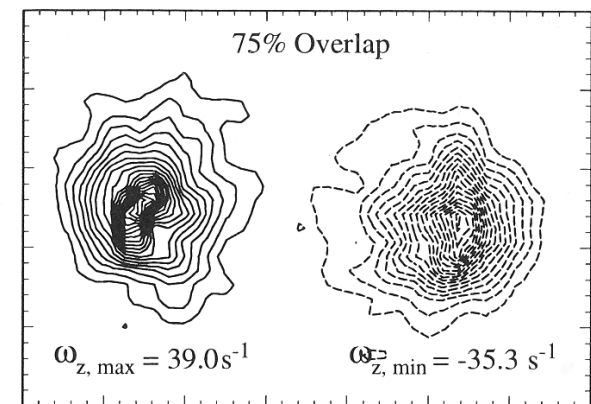
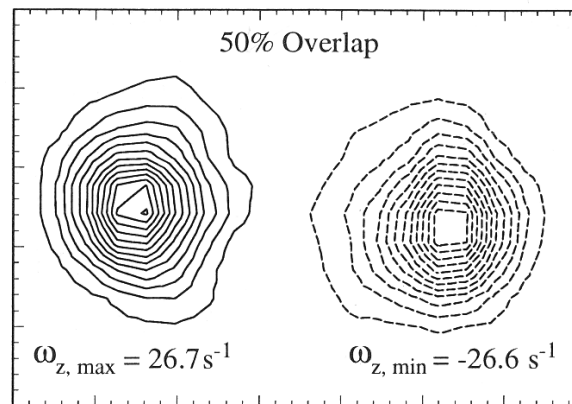
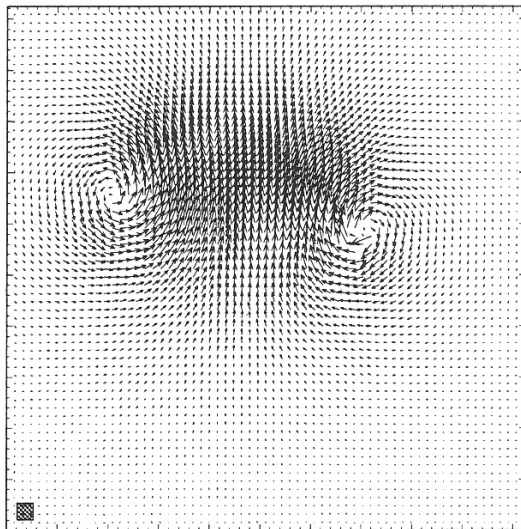
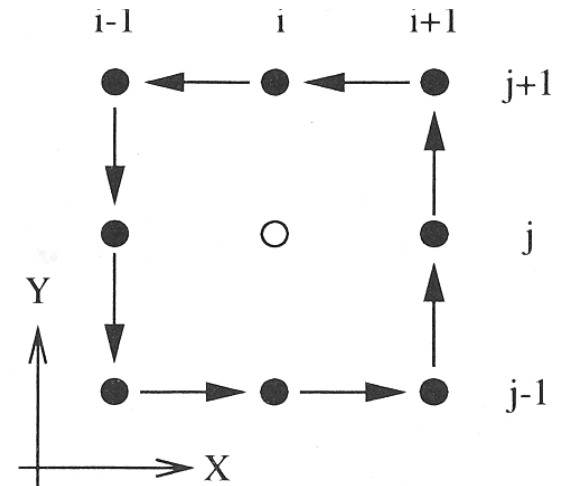
$$\Gamma = -\oint_C \vec{V} \cdot d\vec{l} = -\iint_S \vec{\omega} \cdot d\vec{A}$$

$$\Rightarrow \omega_z = \frac{\Gamma_{x-y}}{dA}$$

$$(\omega_z)_{i,j} \cong \frac{\Gamma_{i,j}}{4\Delta X \Delta Y}$$

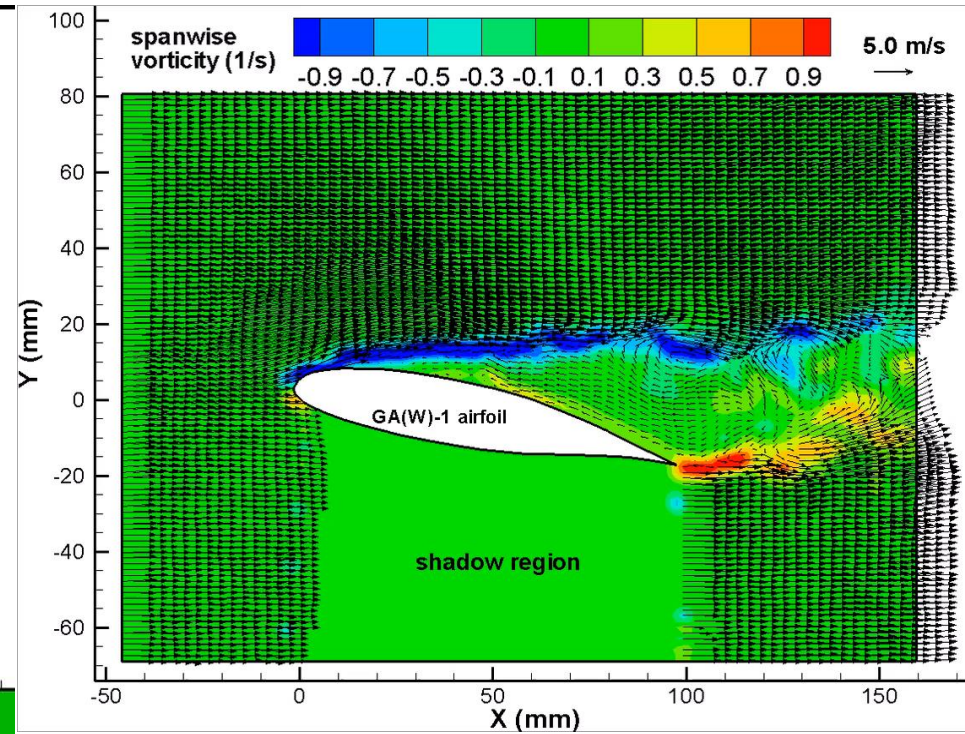
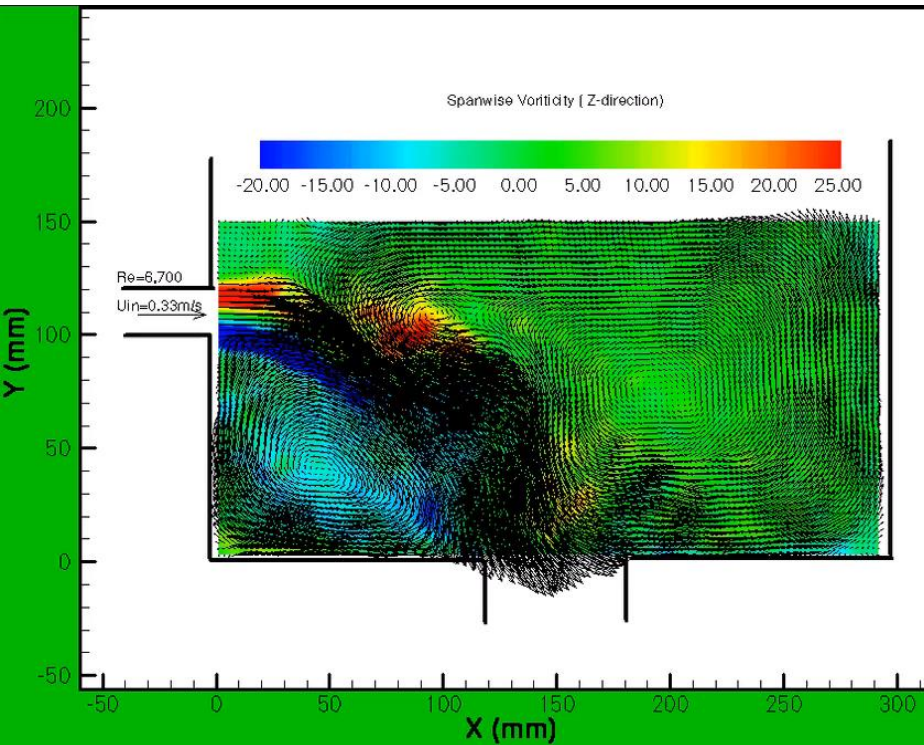
with

$$\begin{aligned} \Gamma_{i,j} = & \frac{1}{2} \Delta X (U_{i-1,j-1} + 2U_{i,j-1} + U_{i+1,j-1}) \\ & + \frac{1}{2} \Delta Y (V_{i+1,j-1} + 2V_{i+1,j} + V_{i+1,j+1}) \\ & - \frac{1}{2} \Delta X (U_{i+1,j+1} + 2U_{i,j+1} + U_{i-1,j+1}) \\ & - \frac{1}{2} \Delta Y (V_{i-1,j+1} + 2V_{i-1,j} + V_{i-1,j-1}) \end{aligned}$$



**Fig. 6.10.** Vorticity field estimates obtained from PIV velocity fields by the circulation method: (left) the velocity field is twice oversampled, (right) four times oversampled. The contours of this laminar vortex pair are known to be smooth such that the nonuniformities are due to measurement noise

# Vorticity distribution Examples

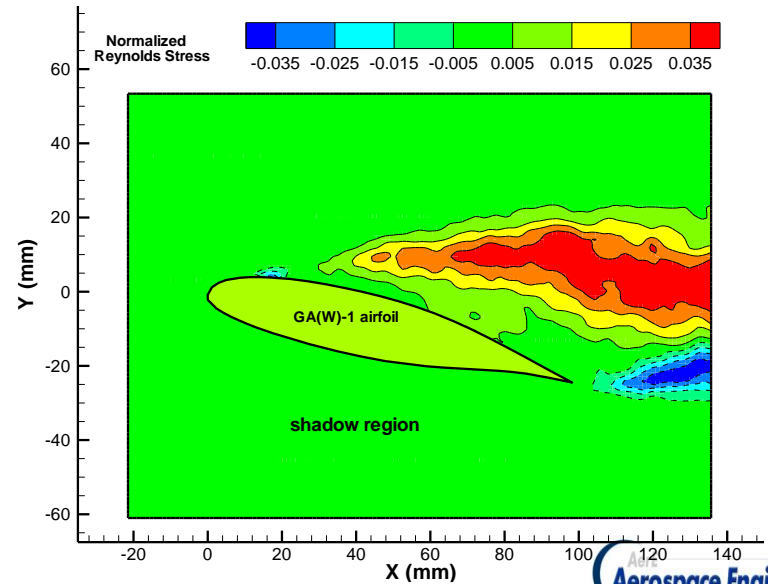
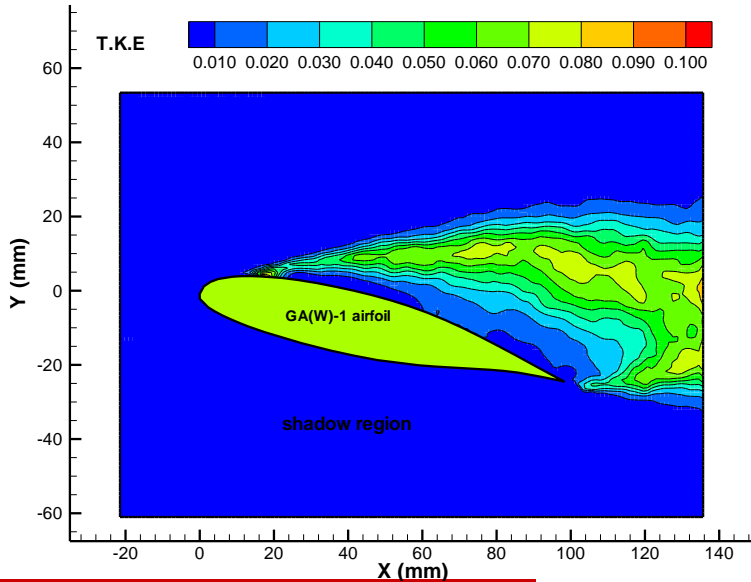
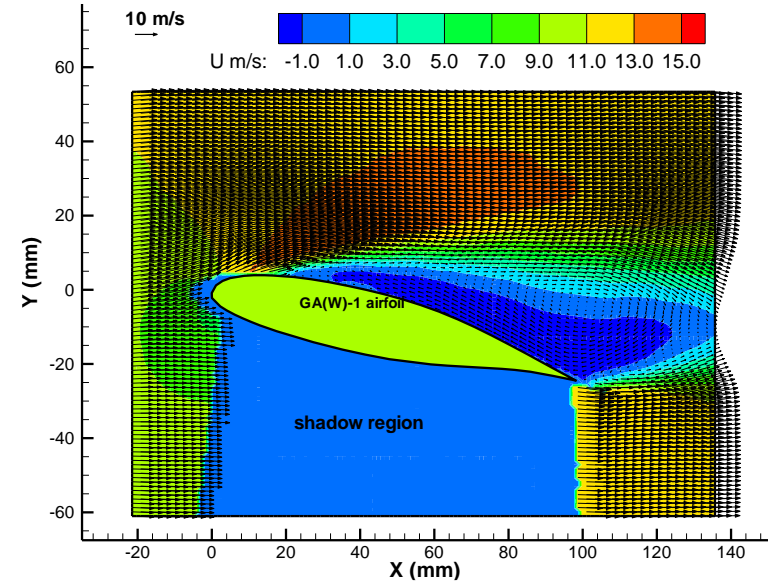
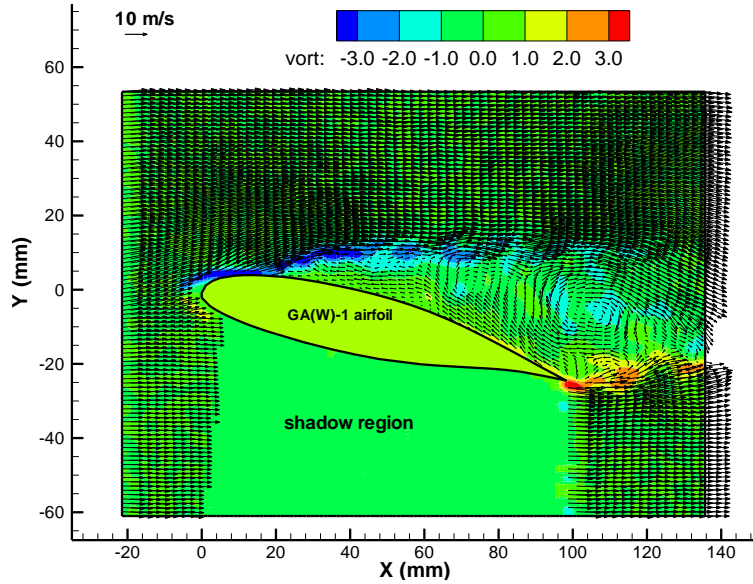




# Ensemble-averaged quantities

- **Mean velocity components in x, y directions:**  $U = \sum_{i=1}^N u_i / N$   $V = \sum_{i=1}^N v_i / N$
- **Turbulent velocity fluctuations:**  $\overline{u'} = \sqrt{\sum_{i=1}^N (u_i - U)^2 / N}$   $\overline{v'} = \sqrt{\sum_{i=1}^N (v_i - V)^2}$
- **Turbulent Kinetic energy distribution:**  $TKE = \frac{1}{2} \rho (\overline{u'^2} + \overline{v'^2})$
- **Reynolds stress distribution:**  $\tau = -\rho \overline{u'v'} = -\rho \sum_{i=1}^N \frac{(u_i - U)(v_i - U)}{N}$

# Ensemble-averaged quantities



# Pressure field estimation

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial x} + \frac{\mu}{\rho} \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} = -\frac{1}{\rho} \frac{\partial p}{\partial y} + \frac{\mu}{\rho} \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right)$$

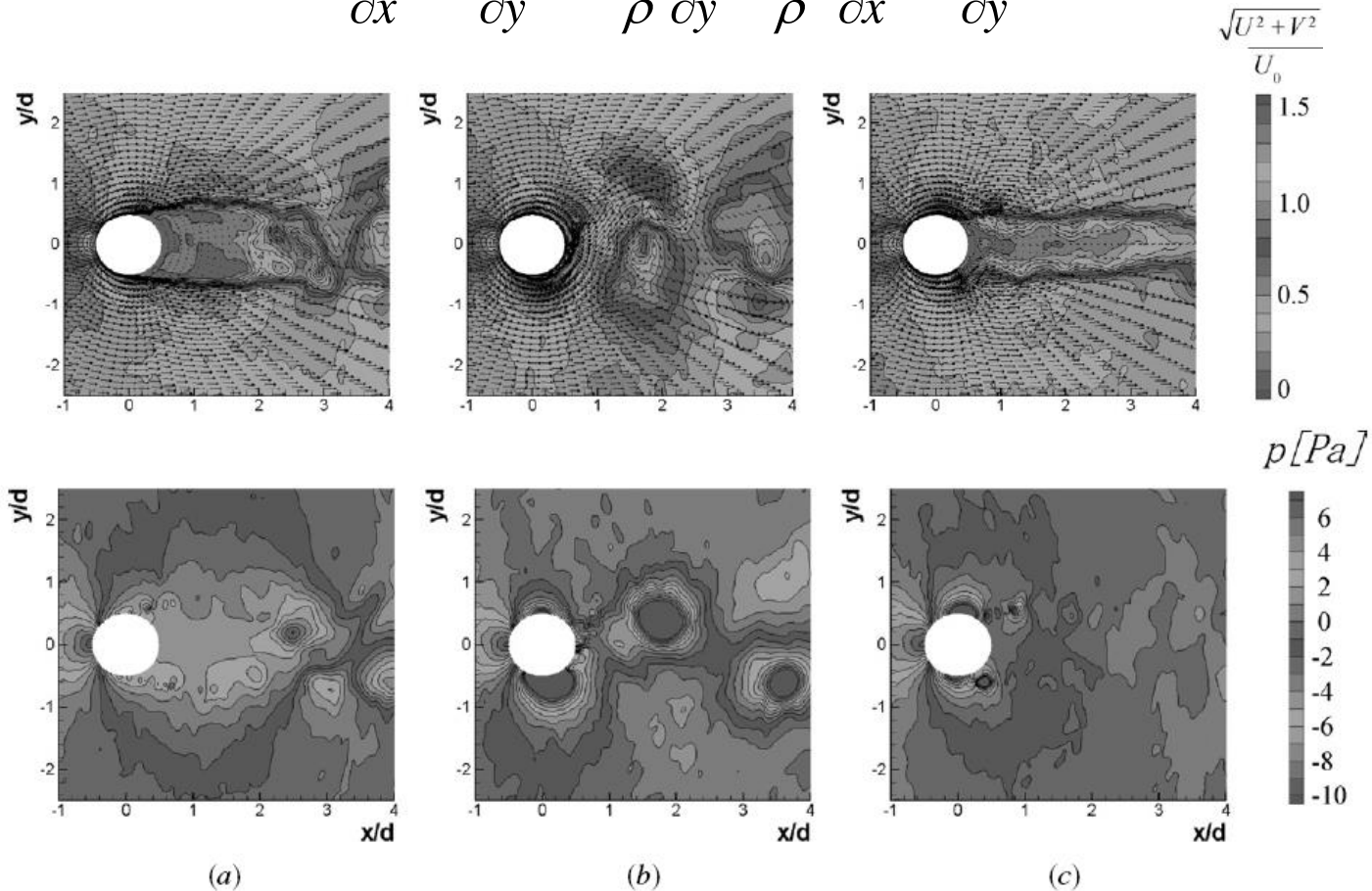
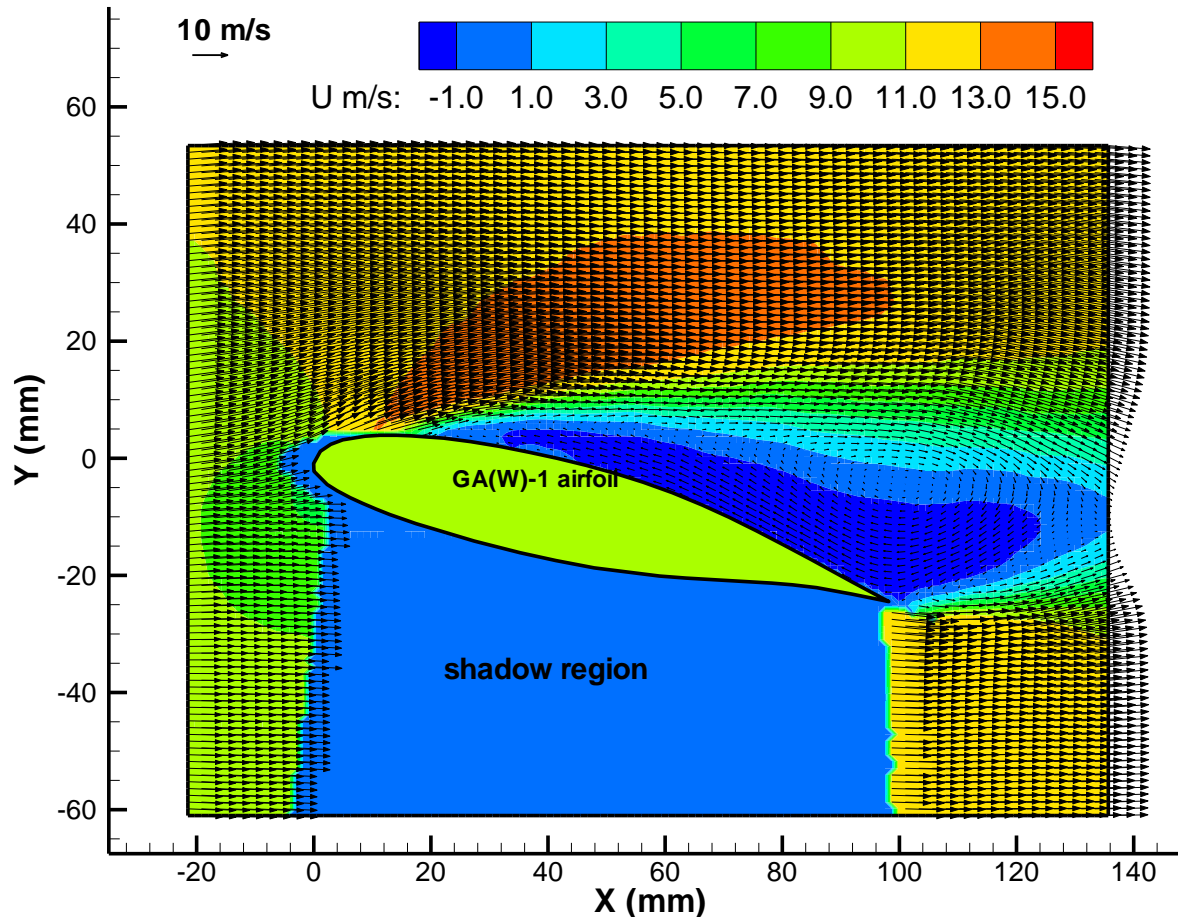


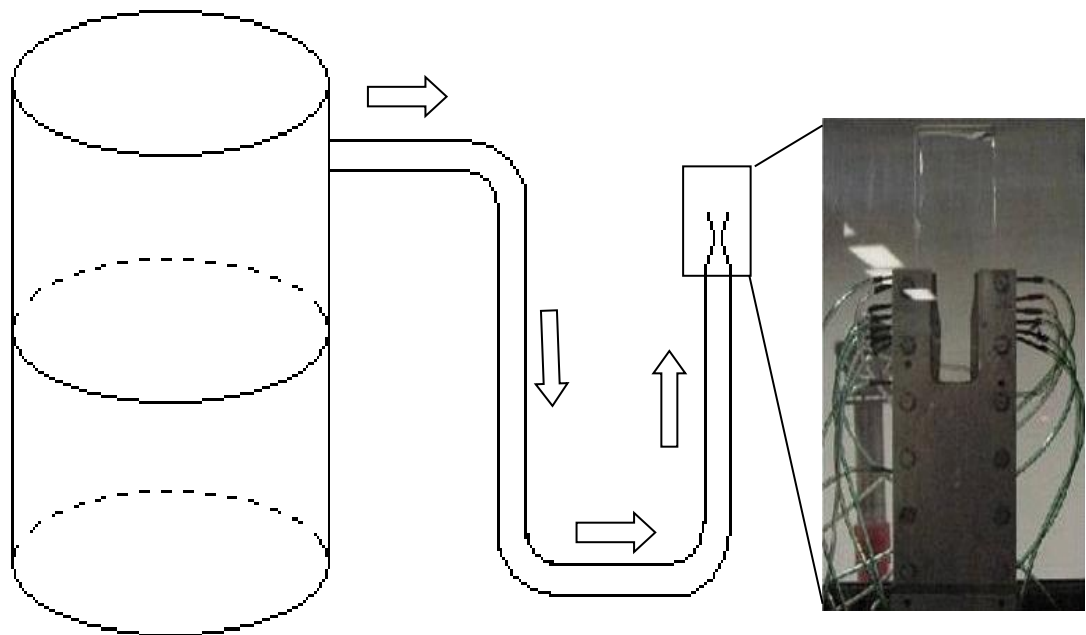
Figure 6. Instantaneous pressure field around a circular cylinder. (a) Stationary cylinder, (b) low-frequency oscillation ( $S_r = 0.2, V_r = 2$ ) and (c) high-frequency oscillation ( $S_r = 1, V_r = 2$ ).

# Integral Force estimation

$$\frac{\partial}{\partial t} \int_{C.V.} \rho \vec{V} dV + \int_{C.S.} (\rho \vec{V} \vec{V}) \cdot d\vec{A} = \int_{C.S.} \tilde{P} \cdot d\vec{A} + \int_{C.V.} \rho \vec{f} dV + \vec{F}$$

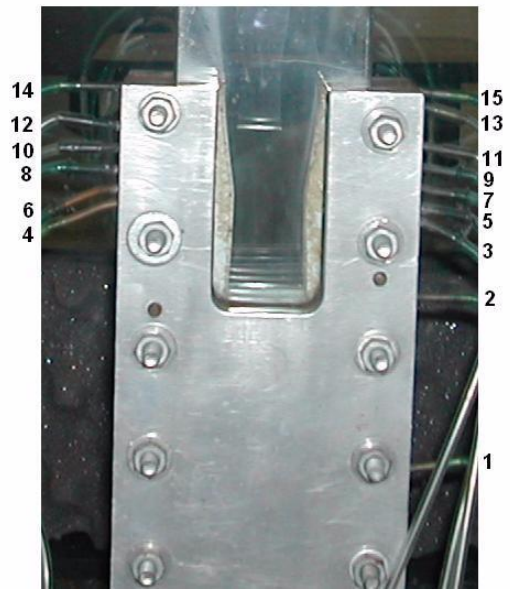


# AerE344 Lab # 10: Pressure Measurements in a de Laval Nozzle



Tank with compressed air

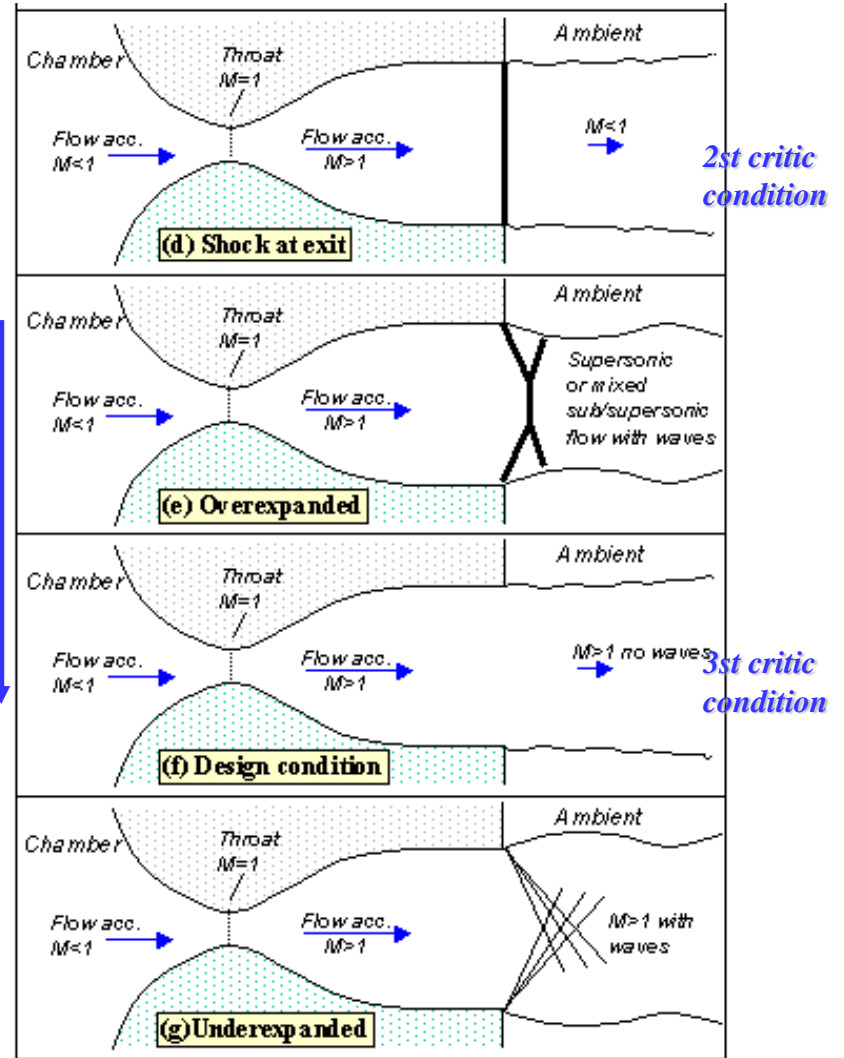
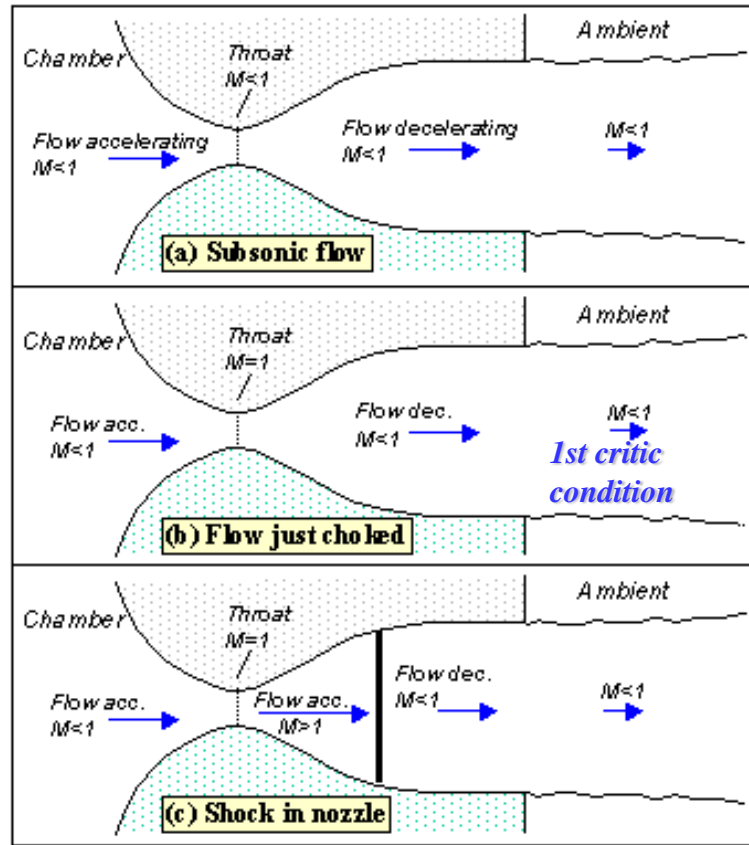
Nozzle Pressure Tap Numbering Diagram



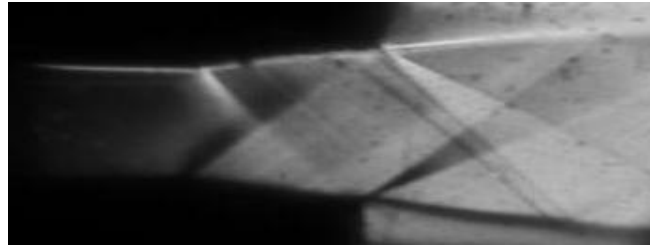
Test section

Tap No.	Distance downstream of throat (inches)	Area (Sq. inches)
1	-4.00	0.800
2	-1.50	0.529
3	-0.30	0.480
4	-0.18	0.478
5	0.00	0.476
6	0.15	0.497
7	0.30	0.518
8	0.45	0.539
9	0.60	0.560
10	0.75	0.581
11	0.90	0.599
12	1.05	0.616
13	1.20	0.627
14	1.35	0.632
15	1.45	0.634

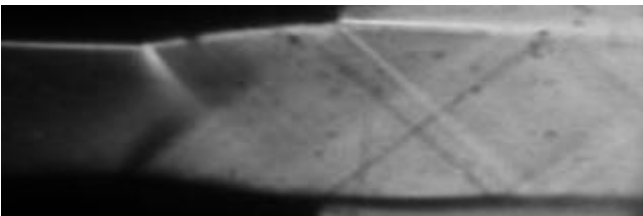
# 1st, 2nd and 3rd critic conditions



# 1<sup>st</sup>, 2<sup>nd</sup>, and 3<sup>rd</sup> critical conditions



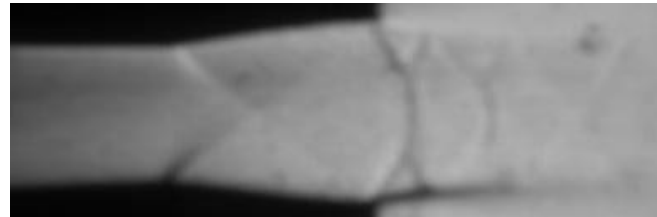
*Under-expanded flow*



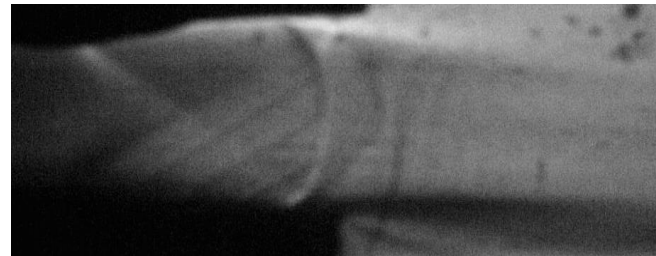
*Flow close to 3<sup>rd</sup> critical*



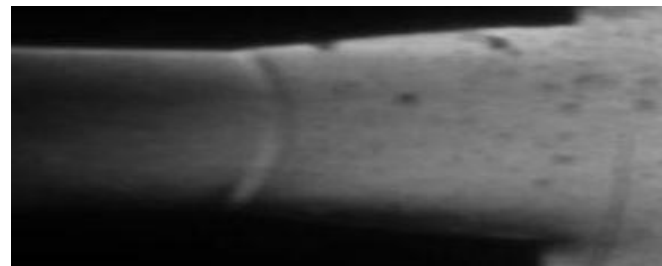
*Over-expanded flow*



*2<sup>nd</sup> critical – shock is at nozzle exit*

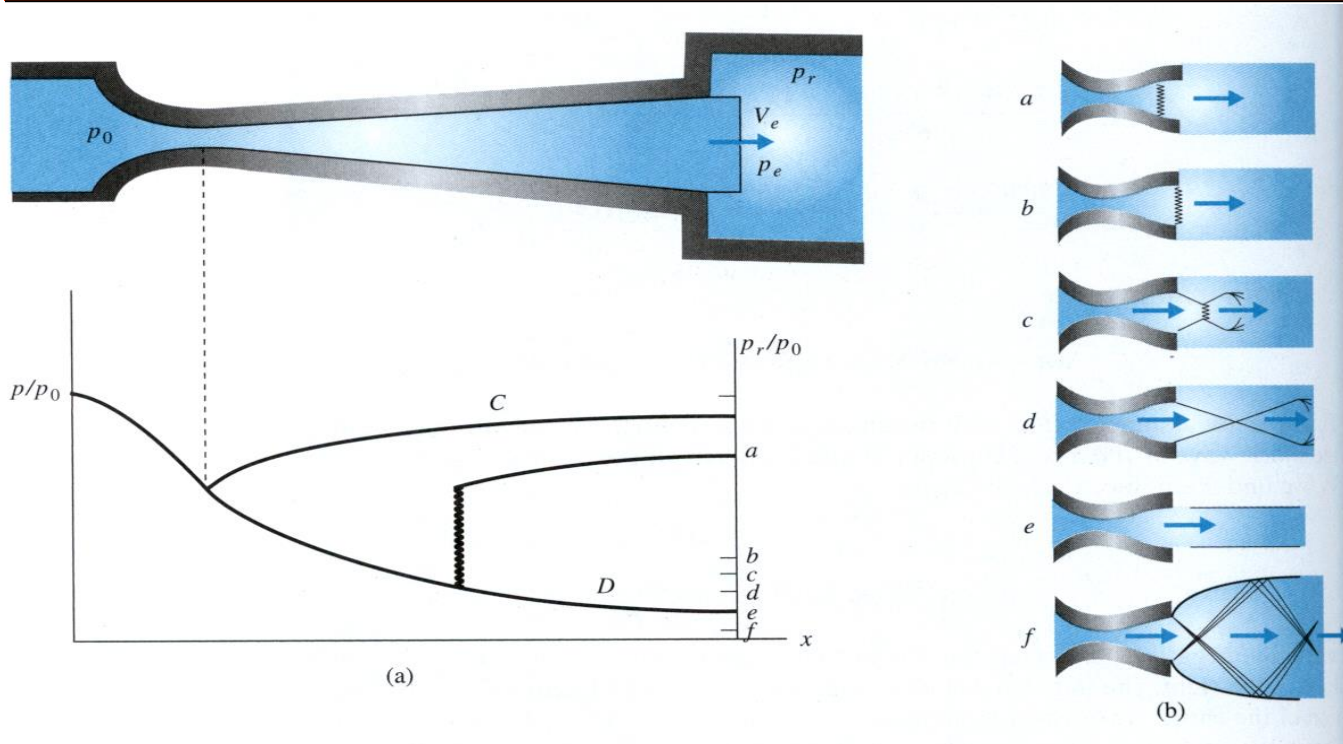


*Over-expanded flow with shock between nozzle exit and throat*



*1<sup>st</sup> critical – shock is almost at the nozzle throat.*

# AerE344 Lab#10: Pressure Measurements in a de Laval Nozzle



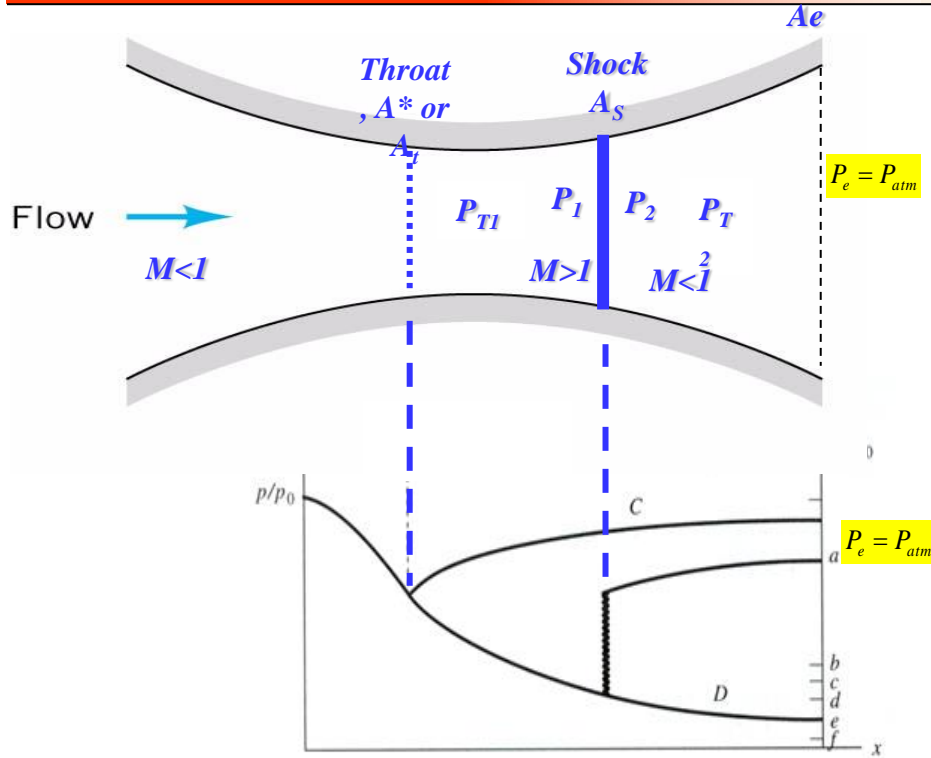
1. Under-expanded flow
2. 3rd critical
3. Over-expanded flow with oblique shocks
4. 2nd critical
5. Normal shock existing inside the nozzle
6. 1st critical

## Required Plots:

- Plots of the measured pressure (static and total pressure) as a function of distance along the nozzle axis for the cases 2, 4, 5 and 6.
- Plots of the theoretically predicted pressure (static and total pressure) as a function of distance along the nozzle axis for the cases 2, 4, 5 and 6.
- Plots with the measured and predicted values of the wall pressure distribution on the same graphs for the cases 2, 4, 5 and 6 for comparison.
- Plots of the theoretically predicted and measured Mach number as a function of distance along the nozzle axis for the cases 2, 4, 5 and 6.



# Prediction of the Pressure Distribution within a De Laval Nozzle by using Numerical Approach



- Using the area ratio, the Mach number at any point up to the shock can be determined:

$$\left(\frac{A}{A^*}\right)^2 = \frac{1}{M^2} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}}$$

- After finding Mach number at front of shock, calculate Mach number after shock using:

$$M_2^2 = \frac{1 + \frac{\gamma-1}{2} M_1^2}{\gamma M_1^2 - \frac{\gamma-1}{2}}$$

- Then, calculate the  $A_2^*$

$$\left(A_2^*\right)^2 = M_2^2 A_s^2 \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M_2^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}}$$

which allows us calculate the remaining Mach number distribution

$$\left(\frac{A}{A_2^*}\right)^2 = \frac{1}{M^2} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}}$$

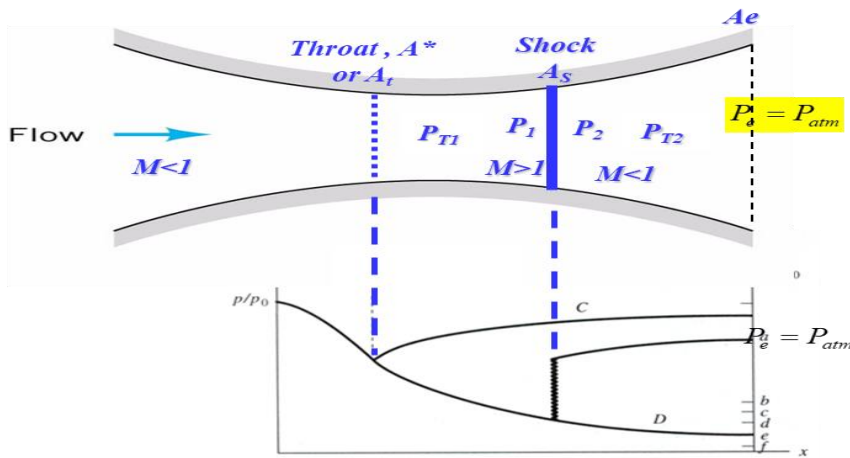
- d. To calculate Mach number given the Mach-Area relation, can use Newton iteration to find M

$$F = \left(\frac{A}{A^*}\right)^2 = M^2 \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}} \quad (2.8)$$

$$F' = \frac{dF}{dM} = \frac{2}{M^3} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}} - \frac{2}{M} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{2}{\gamma-1}} \quad (2.9)$$

$$M^{n+1} = M^n - \frac{F}{F'} \quad (2.10)$$

# Prediction of the Pressure Distribution within a De Laval Nozzle by using Shock Table Method



Tap No.	Distance downstream of throat (inches)	Area (Sq. inches)
1	-4.00	0.800
2	-1.50	0.529
3	-0.30	0.480
4	-0.18	0.478
5	0.00	0.476
6	0.15	0.497
7	0.30	0.518
8	0.45	0.539
9	0.60	0.560
10	0.75	0.581
11	0.90	0.599
12	1.05	0.616
13	1.20	0.627
14	1.35	0.632
15	1.45	0.634

- Method #1: To solve the equation numerically

$$\left(\frac{A}{A^*}\right)^2 = \frac{1}{M^2} \left[ \frac{2}{\gamma+1} \left( 1 + \frac{\gamma-1}{2} M^2 \right) \right]^{\frac{\gamma+1}{\gamma-1}}$$

- Method #2: To use Isentropic Flow properties table (Appendix-A of Anderson's textbook)
  - If the shockwave is located at position of tab#12:

Tap No.	A/A*	Mach #	P/P <sub>t</sub>	P	P <sub>g</sub>
1	1.681	0.37	0.9098		
2	1.111	0.67	0.7401		
3	1.008	0.97	0.5469		
5	1.000	1.00	0.5283		
7	1.088	1.35	0.3370		
9	1.176	1.50	0.2724		
11	1.258	1.61	0.2318		
pre-shock	1.294	1.64	0.2217		
post-shock					
13					
15					

# Examples of the previous lab reports

